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(71) Applicant (for CA only): SCHLUMBERGER CANADA  
LIMITED [CA/CA]; Eau Claire Place I, 525 3rd Avenue,  
SW, Alberta, Alberta T2P004 (CA).

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(71) Applicant (for FR only): COMPANIE DES SERVICES  
DOWELL SCHLUMBERGER S.A. [FR/FR]; 50, Av-  
enue Jean Jaures, F-F-92120 Montrouge (FR).

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(71) Applicant (for AM, AT, AZ, BY, DE, DK, HR, IT, KG, KP,  
KR, KZ, MD, NO, NZ, PL, RO, RU, TJ, TM, UA, ZA only):  
SCHLUMBERGER TECHNOLOGY B.V. [NL/NL];  
Parkstraat 83-89, NL-2514 JG The Hague (NL).

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(71) Applicant (for GB, JP, NL only): SCHLUMBERGER  
HOLDINGS LIMITED [/]; P. O. Box 71, Craigmuir  
Chambers, Road Town, Tortola (VG).

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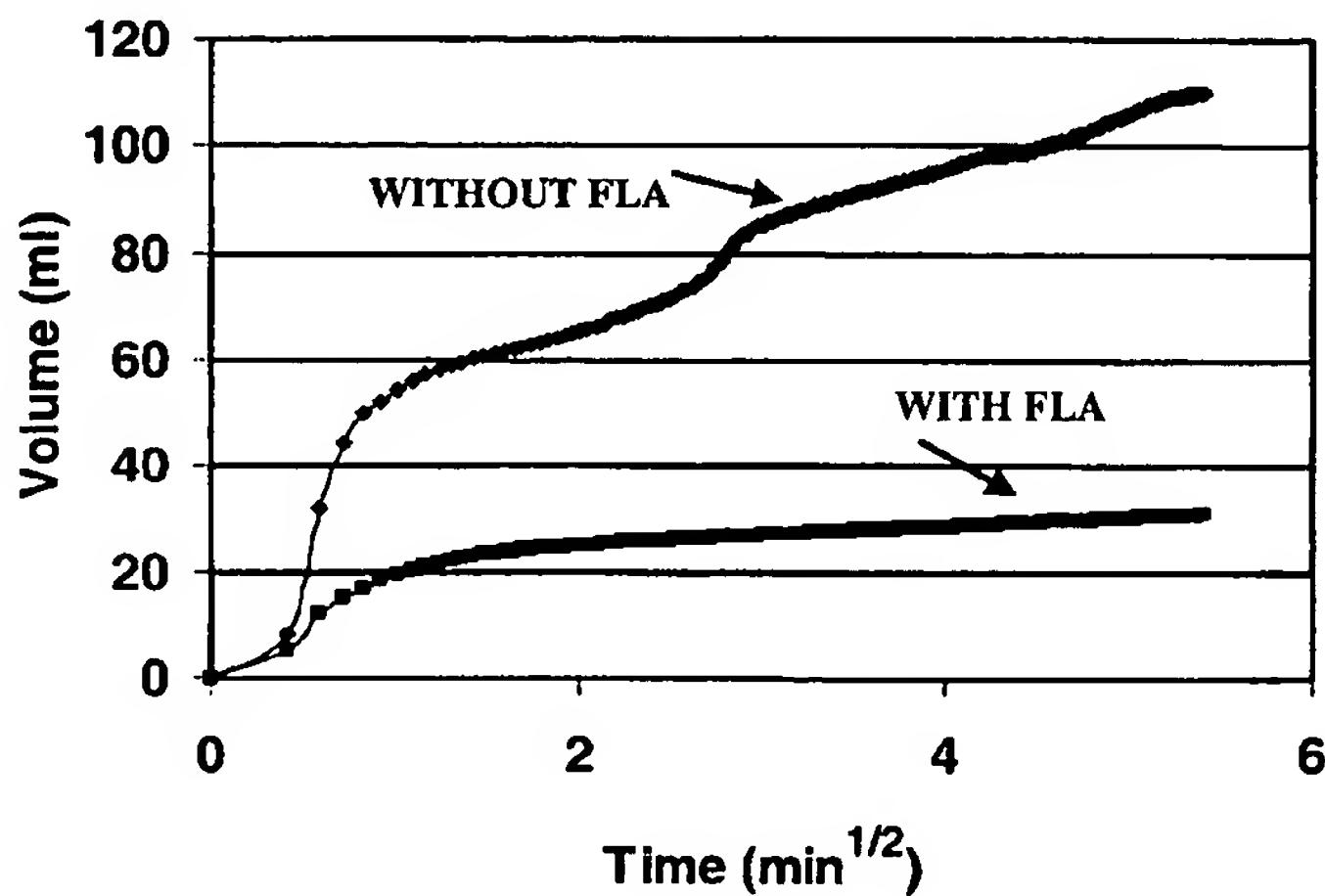
(72) Inventors: BONEY, Curtis, L.; 14918 Chadbourne,  
Houston, TX 77079 (US). WILLBERG, Dean; 3214  
Lakefield Way, Sugar Land, TX 77479 (US). MILLER,  
Matthew, J.; 3054 La Quinta Drive, Missouri City, TX  
77459 (US).

(71) Applicant (for AE, AG, AL, AU, BA, BB, BE, BF, BG, BJ,  
BR, BZ, CF, CG, CH, CI, CM, CN, CO, CR, CU, CY, CZ,  
DM, DZ, EC, EE, ES, FI, GA, GD, GE, GH, GM, GN, GQ,  
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TN, TR, TT, TZ, UA, UG, UZ, VC, VN, YU, ZM, ZW only):  
SOFITECH N.V. [BE/BE]; 140 rue de Stalle, B-B-1180  
Brussels (BE).

(74) Agent: MENES; Etudes et Productions Schlumberger, 1,  
rue Henri Becquerel, BP 202, F-92142 Clamart (FR).

[Continued on next page]

(54) Title: METHODS FOR CONTROLLING SCREENOUTS



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(57) Abstract: Methods are presented to induce a screenout during a subterranean formation fracturing or combined fracturing and gravel packing treatment by laying down a filter cake early in the treatment, then injecting proppant slurry, and then while proppant slurry injection continues chemically damaging the filter cake with one or more filter cake degradation agents, and optional filter cake degradation agent aids, so that leak-off increases, the concentration of proppant in the fracture increases, and the proppant screens out. The additional use of bridging-promoting materials, alone or in conjunction with filter cake degradation, is included.



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## Methods for Controlling Screenouts

### *Technical Field of the Invention*

This Invention relates to increasing the flow of fluids into or out of subterranean wells. More particularly it relates to stimulation of the flow of fluids from the rock of a formation into a wellbore. Most particularly it relates to methods of controlling the size and shape, location, and quality of fractures created in hydraulic fracturing (either conventional or with coiled tubing), in fracturing followed by gravel packing, or in fracturing and gravel packing in one operation.

### *Background of the Invention*

Hydraulic fracturing, gravel packing, or fracturing and gravel packing in one operation, are used extensively to stimulate the production of hydrocarbons, water and other fluids from subterranean formations. These operations involve pumping a slurry of "proppant" in hydraulic fracturing (natural or synthetic materials that prop open a fracture after it is created) or "gravel" in gravel packing. In high permeability formations, the goal of a hydraulic fracturing treatment is typically to create a short, wide, highly conductive fracture, in order to bypass near-wellbore damage done in drilling and/or completion, to ensure good communication between the rock and the wellbore and to increase the surface area available for fluids to flow into the wellbore. Gravel is also a natural or synthetic material, which may be identical to, or different from, proppant. Gravel packing is used for "sand" control. Sand is the name given to any particulate material, such as clays, from the formation that could be carried into production equipment. Gravel packing is a sand-control method used to prevent production of formation sand, in which a steel screen is placed in the wellbore and the surrounding annulus is packed with prepared gravel of a specific size designed to prevent the passage of formation sand that could foul subterranean or surface equipment and reduce flows. The primary objective of gravel packing is to stabilize the formation while causing minimal impairment to well productivity.

Sometimes gravel packing is done without a screen. High permeability formations are frequently poorly consolidated, so that sand control is needed. Therefore, hydraulic fracturing treatments in which short, wide fractures are wanted are often combined in a single continuous ("frac and pack") operation with gravel packing. For simplicity, in the following we may refer to any one of hydraulic fracturing, fracturing and gravel packing in one operation (frac and pack), or gravel packing, and mean them all.

It is very undesirable to allow the proppant or gravel to pack the wellbore above the producing formation. If this happens, the wellbore must be cleaned out to permit various other downhole operations, such as placement of tools, to permit optimal fluid production. It is also very undesirable if the operation screens out too late or not at all, that is if the fracture keeps growing, in length and/or in height, beyond what is necessary and desired, and an optimal pack and desired fracture size and shape are never generated to maximize production and to prevent flowback of proppant or sand.

As mentioned, short, wide fractures are often desired. However, these are not always obtained by conventional fracturing treatments. The most common method of deliberately creating short-wide fractures is to initiate a tip screenout (TSO) during the pumping operation. In a tip screenout, the solids concentration at the tip of the fracture becomes so high due to fluid leak-off into the formation that the slurry is no longer mobile. The concentrated proppant slurry plugs the fracture, and prevents additional fracture growth. Additional pumping of the proppant/fluid slurry into the formation after the screenout causes the fracture to grow wider, and large concentrations of proppant per surface area are placed in the fracture. The design of these treatments relies heavily on knowing the correct mechanical properties, permeability, reservoir pressure and fluid saturations of the formation being treated. Prior to most of these treatments a small fracturing treatment (sometimes called a "data frac" or "mini-frac") is performed in order to measure these properties and to determine the formation's response to a hydraulic fracturing treatment. Treatment designs are often modified on the fly to incorporate this new information. Important design parameters are the size of the pad, the size and number of stages, and the proppant or gravel concentration in each subsequent stage, and the nature of the fluid and additives used in each stage. Treatment design and modification is typically done with the aid of a computer model, many of which are available in the industry.

The pad is the proppant-free fluid pumped to initiate and propagate a fracture before stages including proppant or gravel are started. It typically serves another purpose as well. It typically lays down a

coating, called a “filter cake”, on the faces of the forming fracture. This filter cake reduces the flow of fluid from the fracture into the formation (affecting the “efficiency” of the job (see below)). The filter cake may be formed from the viscosifying agents that are normally present, such as polymers. The filter cake may also be formed by adding additional materials to the fluid for that purpose, especially if the pores in the fracture face are large. Such optionally added materials in this use are often called fluid loss control additives, or FLA's.

In hydraulic fracturing, in particular in low permeability formations where the longest possible fracture is desired (in order to create the largest possible fracture face for flow of fluids into the fracture and ultimately into the wellbore), modes of operation that might induce a tip screenout are typically avoided, in order to achieve long, conductive fractures. If a tip screenout is encountered in such a fracturing operation before the entire designed treatment is pumped, as inferred from an increase in pumping pressure, the pump rate is reduced or most likely the treatment is stopped and considered a failure. We will call hydraulic fracturing job designs and job executions in which a tip screenout is not desired and does not occur, “conventional” hydraulic fracturing.

On the other hand, sometimes tip screenouts are desired. Design features typically employed in those special situations in which a tip screenout is desired typically involve methods of ensuring that fluid leak-off is high relative to the rate and amount of proppant injection. This can be achieved by using a small pad, using little or no fluid loss additive, using higher proppant concentrations earlier in the treatment, pumping more slowly, and other methods known to those skilled in the art of fracturing and combined fracturing/gravel packing.

Unfortunately, in spite of data-fracturing information, the pressure transients collected by downhole pressure gauges during treatments indicate that TSO's do not occur in many, perhaps the majority, of the treatments in which they are desired and intended. The fluid at the tip of the fracture remains mobile, the fracture tip continues to grow throughout the treatment and the desired proppant concentration in the fracture is not reached. Therefore, a long, thin fracture is formed and the desired fracture conductivity is not obtained. Often, TSO's have to be coaxed by lowering pump rates or increasing proppant concentrations when the TSO is desired.

There are two principal reasons for not achieving an appropriate TSO. First, the fracture may be too large for the proppant volume. This occurs a) when the pad is too large or b) when the “efficiency” is

too high, or c) when the ratio of proppant volume to slurry volume selected in the design of the job is not high enough. (The "efficiency" in a fracturing operation is high when fluid leak-off is controlled – either naturally by the properties of the fluid and the matrix, or by the addition of fluid loss control additives – to an acceptably low level; efficiency is low when leak-off is high, so that very large volumes of fluid must be pumped in order to generate the intended fracture size and shape and to place a specified amount of proppant or gravel.) Second, the fracture width may be too great for the proppant to form a bridge in the fracture. This may be due to bad initial design (for example in choice of proppant diameter) or to width growth beyond what was expected.

Up until now, besides designing the job better, the major way to deal with these problems was directed towards optimizing the choice of fluid loss control additive or additives and the stages of the job in which they were used, especially if the main problem was that the fracture was too large for the proppant volume.

Fibers are used in fracturing to control proppant flowback. In that case, fiber is added at an optimal concentration to control proppant flowback, while not significantly impacting fracture conductivity. If one is using glass fibers, for example, this concentration is approximately 1 weight per cent by weight of the proppant. This concentration is insufficient to cause bridging during pumping under the conditions at which it is normally employed, especially in low permeability formations. Fibers are also used sometimes to aid in transport of proppant when the viscosity of the fluid is very low. Tip screenout is commonly deliberately avoided in these treatments; proppant concentrations are kept low through careful pre-treatment job design, especially in careful selection of pumping schedules. For example, in these treatments the pad volume is increased over conventional job designs to ensure that sufficient fracture width is generated prior to the proppant/fiber slurry entering the fracture.

The ability to achieve success in obtaining TSO's is very uncertain in significant part due to the fact that the true nature of the subterranean formation is unknown and variable. It would be highly desirable if methods were available to induce a TSO when needed that depended more upon features of the job under the operator's control (especially the chemistry of the fluids and fluid loss control additives used) than on the unknown variability of the formation. There is a need for more reliable ways to ensure that intended tip screenouts will occur and to allow for more flexibility in design of tip screenout treatments.

*Summary of the Invention*

In one embodiment, tip screenouts are induced when desired by adding bridging-promoting agents to the proppant slurry. In another embodiment the bridging-promoting agents are fibers that are added to the proppant slurry at higher concentrations than are normally used for flowback control and the fibers are added early in the treatment to initiate proppant bridging and cause a tip screenout during pumping. Another embodiment of this Invention is deliberately to induce tip screenouts by the use of high concentrations of bridging-promoting agents early in stimulation treatments. Another embodiment of this Invention is deliberately to induce tip screenouts by the use of high concentrations of bridging-promoting agents early in the treatment in combination stimulation/gravel packing treatments, in particular hydraulic fracturing/gravel packing. It is a further embodiment of this Invention deliberately to induce tip screenouts by the use of high concentrations of bridging-promoting agents early in a treatment in combination stimulation/gravel packing treatments in which annular screens are used. Yet another embodiment of this Invention is to use an appropriate choice of treatment parameters to induce tip screenouts but in addition to use high concentrations of bridging-promoting agents early in treatments to increase the probability that a tip screenout will occur. Yet other embodiments are the preceding methods in which bridging-promoting agents are added later in the treatment. Another embodiment is a proppant slurry containing sufficient bridging-promoting agent to cause the slurry to screen out when injected into a fracture.

Another embodiment of the Invention is a method of causing a screenout, during stimulation of a subterranean formation by propped fracturing, by forming a filter cake and then degrading the filter cake with a filter cake degradation agent or agents while injecting proppant slurry into the fracture. In some embodiments the filter cake is formed from the viscosifier for the carrier fluid in the slurry or from a fluid loss additive or both. In some embodiments the filter cake degradation agent may be an oxidizer, an enzyme, an acid or mixtures of these. Another embodiment is a method of causing a screenout in a subterranean formation stimulation treatment, including injecting a slurry of a proppant in a carrier fluid above fracturing pressure to create one or more fractures, the method including the steps of injecting a pad fluid that forms a filter cake; injecting one or more first slurry stages comprising a proppant in a carrier fluid; and degrading the filter cake with a filter cake degradation agent while injecting one or more second slurry stages comprising a proppant in a carrier fluid. In

other embodiments of this method, the pad fluid includes one or more than one of fluid loss additives, filter cake degradation agents, filter cake degradation agent aids, and mixtures thereof, provided that no filter cake degradation agent aid is included for a filter cake degradation agent that is included; the one or more first slurry stages include one or more than one of fluid loss additives, filter cake degradation agents, filter cake degradation agent aids, and mixtures thereof, provided that no filter cake degradation agent aid is included for a filter cake degradation agent that is included in the first slurry stages or was in the pad; and the one or more second slurry stages include one or more than one of filter cake degradation agents, filter cake degradation agent aids, and mixtures thereof. In another embodiment, the pad fluid and the one or more first slurry stages each include a fluid loss additive, a first filter cake degradation agent and a filter cake degradation agent aid for a second filter cake degradation agent that is more active under treatment conditions than is the first filter cake degradation agent; and the one or more second slurry stages contain the second filter cake degradation agent. In another embodiment, the filter cake includes a polymer subject to enzymatic and oxidative degradation under treatment conditions; the first filter cake degradation agent is present in the pad and includes an enzyme that degrades the polymer; the second filter cake degrading agent is present in the one or more second slurry stages and includes an oxidizing compound that degrades the polymer; and the second filter cake degradation agent aid for the second filter cake degradation agent is present in one or more than one of the pad fluid, the one or more first slurry stages, and the one or more second slurry stages and is a tertiary amine. In another embodiment the filter cake includes an acid-soluble solid particulate compound and the second filter cake degrading agent is present in the one or more second slurry stages and includes an acid capable of dissolving at least part of the acid-soluble solid particulate compound under treatment conditions. In another embodiment one or more of the pad fluid, the one or more first slurry stages, and the one or more second slurry stages include a bridging-promoting material. In a preferred embodiment, the filter cake includes a polymer subject to enzymatic and oxidative degradation under treatment conditions; the first filter cake degradation agent is present in the pad and includes an enzyme that degrades the polymer; the second filter cake degrading agent is present in the one or more second slurry stages and includes an oxidizing compound that degrades the polymer; the second filter cake degradation agent aid for the second filter cake degradation agent is present in one or more than one of the pad fluid, the one or more first slurry stages, and

the one or more second slurry stages and is a tertiary amine; and at least some of the one or more first slurry stages contain a bridging-promoting material. In other embodiments, a sand control screen is in place before the treatment. In other embodiments, the treatment is a combined fracturing/gravel packing treatment. It is a further embodiment of the Invention to provide ways to induce tip screenouts in treatments in which it would otherwise have been difficult, or expensive, or inefficient, or even impossible, to do so, thus giving the operator additional means to control the treatment.

#### *Brief Description of the Figures*

Figure 1 shows typical fluid leak-off volume data with and without a fluid loss additive.

Figure 2 is a schematic of the depth of penetration of leaked-off fluid into a formation with and without a leak-off additive.

Figure 3 shows dynamic fluid loss volume and fluid viscosity vs. a time function in experiments with two different combinations of FLA, filter cake degradation agents, and a filter cake degradation agent aid.

Figure 4 shows dynamic fluid loss volume and fluid viscosity vs. a time function in an experiment in which addition of FLA is stopped and there is no filter cake degradation agent or filter cake degradation agent aid.

Figure 5 is a schematic showing the effect on fracture generation of adding an FLA, fiber, filter cake degradation agents, and a filter cake degradation agent aid.

#### *Detailed Description of Preferred Embodiments*

To help in understanding deliberate tip screenouts promoted by job design in hydraulic fracturing and combined fracture/gravel packing operations, see M. Economides and K. Nolte, eds., *Reservoir Stimulation*, 3<sup>rd</sup> edition, John Wiley & Sons, Ltd, New York (2000) pp 10-21 to 10-24; and F. L. Monus, F. W. Broussard, J. A. Ayoub and W. D. Norman, "Fracturing Unconsolidated Sand Formations Offshore Gulf of Mexico," SPE 24844, (1992). We have now found that we can create a situation in which a slurry in a fracture is no longer mobile by changing one or both of two properties of the slurry. The solids may be altered, by addition of a solid material other than proppant, so that the

slurry is no longer mobile at a lower concentration than that at which it would no longer be mobile without the addition of the material, or fluid leak-off may be increased so that the solids concentration is increased, or both. We have found ways to bring about screenouts in a fracture deliberately and in a controlled manner by manipulation of the composition of the injected fluids and/or by adding bridging-promoting materials such as fibers. One method is particularly effective when the failure to screen out is due to the fracture being too large for the proppant volume; this method is to form a filter cake and then to reduce the amount of filter cake, or increase its permeability, at the appropriate time. We will use the term filter cake degradation to encompass reducing the amount of filter cake or increasing its permeability by breaking or dissolving at least a portion of at least one of the components of the filter cake. This is done, for example, by breaking or dissolving the filter cake during the job with one or more appropriate breakers or dissolvers, which we will term filter cake degradation agents, sometimes with an additional breaker or dissolver aid, which we will term a filter cake degradation agent aid. The breakers or dissolvers may be delayed, for example with delay agents or by encapsulation. When the fracture is too large for the proppant volume, one or more breakers or dissolvers may be added throughout the job or at least in the pad and/or early stages of the job.

Other methods are particularly effective when the failure to screen out is due primarily to the fracture being too wide for the proppant to bridge. An example is to reduce the efficiency in the later stages of the job by adding an appropriate breaker, sometimes with a breaker aid, in the later stages of the job, or by adding more breaker or a better breaker in the later stages of the job. In this embodiment, breaker may not have been used in the pad or in the early proppant stages. These breakers are effective when the filter cake's resistance to fluid flow results primarily from polymers in the fluid or in the FLA.

If the filter cake's resistance to fluid flow results primarily from calcium carbonate or one or more other acid-soluble materials in the FLA, the filter cake can be dissolved by adding acid to the later stages.

Another method is to add fibers or other materials (termed bridging-promoting materials) with the proppant to assist in bridging, alone or in conjunction with one of the above methods of breaking or dissolving the filter cake. Screenouts begin with bridging, that is solids in the fracture cease moving while the liquids can continue to flow; important parameters affecting bridging propensity at a given location in the fracture are particle size and shape distribution, fracture width and the volume concentration of proppant in the slurry. Addition of bridging-promoting materials affects

bridging directly; deliberate destruction of the filter cake during the treatment affects the proppant concentration.

The methods involving breaking or dissolving the filter cake and adding fibers can be combined, simultaneously or consecutively. These methods can also be used to form wider fractures (that have greater fracture conductivity) deliberately. These methods can also be used as a form of diversion, that is the operator can deliberately stop the growth and packing of one fracture and initiate a new fracture without zonal isolation. The methods can be used to destroy the FLA throughout the fracture or only in part of it. The operator can decide and control when and where the screenout occurs (and avoid the undesirable results of failure to screen out, of very gradual and inefficient screenout, or of screenout in the wellbore above the formation) by accelerating the leak-off, optionally also by assisting bridging.

The underlying and unifying concept of methods involving filter cake degradation, is that a filter cake is laid down early in the treatment, then proppant slurry is injected, and then while proppant slurry injection continues the filter cake is chemically damaged by a filter cake degradation agent so that leak-off increases, the concentration of proppant in the fracture increases, and the proppant screens out. Depending upon such factors as the reactivity under the treatment conditions (for example temperature and carrier fluid pH) of the filter cake degradation agent or agents used, the thickness of the filter cake deposited (affected for example by the carrier fluid viscosity and the formation permeability) and other job design parameters such as the planned duration of the job, dimensions of the fracture, and proppant particle size, the timing of the addition of various chemicals will vary. For example, the pad must be pumped long enough and/or contain enough FLA to ensure laying down the needed filter cake. The filter cake degradation must not be so fast, or be begun so soon, that screenout occurs before it is wanted. Conversely, the filter cake degradation must not be so slow, or be begun so late, that screenout does not occur or occurs too late. Proppant addition is usually done in stages. In each stage a certain proppant concentration is injected for a certain amount of time. Successive stages usually have successively increasing proppant concentrations. The proppant concentration may also be ramped smoothly, that is increase continuously during the proppant-laden stages. To aid in description, a typical job will be broken up into the pad and two sets of proppant slurry stages. In the pad, the fracture is initiated and filter cake is laid down. In the first set of stages, the fracture is enlarged. In the second set of stages, a screenout occurs and the fracture is packed with proppant. As was said, certain other features of the job may strongly influence the timing of the addition of the

chemicals. If the pad must be small, laying down of filter cake may continue in all of, or the early stages of, the first set of stages. If the filter cake degradation agent is slow acting, addition may begin even in the pad, and degradation may begin in the first set of stages. If it is very fast acting, addition may begin only in the second set of stages. Filter cake degradation agents of successively increasing reactivity may be used, or filter cake degradation agents that degrade different components of the filter cake may be used simultaneously or successively. If the filter cake degradation agent is not reactive enough a filter cake degradation agent aid may be added. That filter cake degradation agent aid may be added before or after the filter cake degradation agent is added, in such a way that both are present only in the second set of stages, or they may both be added together in the second set of stages. A bridging-promoting agent may be added in any or all of the pad and stages. One skilled in the art of subterranean formation stimulation could design treatments that generate a fracture having specific final parameters (such as dimensions and conductivity) in many different ways within the scope and spirit of the Invention, depending upon such factors as, for example, the availability of chemicals and materials; the availability and capability of the equipment with which the chemicals and materials can be added; and cost.

The Invention is preferably carried out by first considering information about the well, the formation, the fluids available, and criteria for a successful fracture stimulation, and preparing an optimized plan for maximizing stimulated well performance according to the data and the criteria. Such a design will include injection of an amount of a selected pad fluid and an amount of a selected fracture fluid. This is usually done by analyzing the well using fracturing design and evaluation software in which pressure gradients are combined with fracture length and height evolution algorithms, complete leak-off information, and the effects of multiple fluid injections and their temperature changes. For hydraulic fracturing or gravel packing, or a combination of the two, aqueous fluids for pads or for forming slurries are viscosified with polymers (usually crosslinked with a boron, zirconium or titanium compound), or with viscoelastic surfactant structures ("VES's") that can be formed using certain surfactants that form appropriately sized and shaped micelles. Any fracture or gravel packing fluids can be used in the Invention, provided that they are compatible with the special materials of the Invention (FLA's, fibers, breakers, breaker aids), and with the formation, the proppant, and the desired results of the treatment. Thus the fluid may for example be aqueous based or oil-based, acidic or basic, and may comprise one or more polymers, viscoelastic surfactants, or gelled oils. The polymers may be crosslinked. The methods of the Invention may be incorporated into the original job design or the job

may be designed without planning a TSO and then it may be decided during the job execution that a TSO is desired and the job may be modified on the fly accordingly. (Note that in this description, we often refer to any screenout in the fracture as a tip screenout (TSO), but by TSO we mean a screenout that occurs in the fracture and not necessarily at the very end of the fracture farthest from the wellbore; what is critical is that the screenout occurs when and where it is desired and not in the wellbore.)

We use the term “conventional fracturing” here to refer to hydraulic fracturing in which a tip screenout is neither intended nor desired. We use the term “tip screenout” to mean a screenout that is in the fracture and not in the wellbore, but is not necessarily in the end of the fracture away from the wellbore. In conventional fracturing, modes of operation that might induce a tip screenout are avoided. If a tip screenout is encountered in a conventional fracturing operation, as inferred from an increase in pumping pressure, before the entire designed treatment is pumped, some change(s) may be made on the fly in the job parameters, for example pump rate or proppant concentration, to try to minimize the tendency toward tip screenout. Frequently, however, the treatment is stopped and considered to be a failure.

The pad of the Invention comprises a carrier fluid and a viscosifying polymer or a VES. It may additionally contain other additives normally used in such fluids, provided that none of the components of the pad is deleterious to the formation or to the fracture fluid. Fluids used as the pad in the present Invention may typically contain materials such as corrosion inhibitors, friction reducers, clay stabilizers, scale inhibitors, biocides, and the like.

The carrier fluid provides a medium for the transport of the other components into the formation. Preferably, the carrier fluid is water or brine. Selected organic or inorganic salts or mixtures may be included, provided that they are compatible with all components in the pad, the fracture fluid, the formation and the formation fluids. Solutions containing from about 1 to about 7 % by weight potassium chloride (KCl) or ammonium chloride are often used as the base liquid in fracturing fluids and pads to stabilize clays and prevent clay swelling. Sometimes other brines or seawater may be used. An organic cation salt, such as, in particular, tetra methyl ammonium chloride, is an effective salt, especially but not limited to about 0.2 to about 0.5 percent by weight.

Typically, if a polymer is used to viscosify the fluids, the polymer is water-soluble. Common classes of effective water-soluble polymers include polyvinyl polymers, polymethacrylamides, cellulose

ethers, polysaccharides, lignosulfonates, and ammonium, alkali metal, and alkaline earth salts thereof. Specific examples of typical water soluble polymers are acrylic acid-acrylamide copolymers, acrylic acid-methacrylamide copolymers, polyacrylamides, partially hydrolyzed polyacrylamides, partially hydrolyzed polymethacrylamides, polyvinyl alcohol, polyvinyl acetate, polyalkyleneoxides, carboxycelluloses, carboxyalkylhydroxyethyl celluloses, hydroxyethylcellulose, galactomannans (e.g., guar gum), substituted galactomannans (e.g., hydroxypropyl guar, carboxymethyl hydroxypropyl guar, and carboxymethyl guar), heteropolysaccharides obtained by the fermentation of starch-derived sugar (e.g., xanthan gum), and ammonium and alkali metal salts thereof. Preferred water-soluble polymers include hydroxyethyl cellulose, starch, scleroglucan, galactomannans, and substituted galactomannans.

The optimal polymer concentration can be determined by choosing the desired leak-off parameters and measuring leak-off with samples of the intended fluids and of the formation or of a rock similar to the formation. Leak-off is defined by three terms: "spurt", which is the initial rapid leak-off of fluid before a filtercake barrier is formed on the fracture face and is measured in gallons/100 square feet, and, for the subsequent leak-off that occurs even after a filtercake is formed and is governed by the viscosity and the wall-building propensity:  $C_w$ , the wall-building fluid loss coefficient, and  $C_v$ , the viscosity controlled fluid loss coefficient.  $C_w$  is not applicable where there is no wall-building material present.  $C_v$  is not applicable where there is a low, finite  $C_w$ .  $C_w$  and  $C_v$  are measured in  $\text{ft}/\text{min}^{1/2}$ . Preferred values of spurt,  $C_w$  and  $C_v$  respectively are 0 to about 5, about 0.001 to about 0.05, and about 0.001 to about 0.05; more preferred values are 0 to about 2, about 0.001 to about 0.008, and about 0.001 to about 0.008; most preferred values are 0 to about 1, about 0.001 to about 0.003, and about 0.001 to about 0.003. The values of these parameters (and the actual behavior they represent) can vary significantly provided that a suitable filter cake is produced in an appropriate time. A test method for determining these values is given in Navarrete, R. C., Caweizel, K. E., and Constien, V. G.: "Dynamic Fluid Loss in Hydraulic Fracturing Under Realistic Shear Conditions, in High-Permeability Rocks," SPE Production and Facilities, pp 138-143 (August, 1996).

Any VES based fluid can be used, in and/or after the pad, that is compatible with the formation, the formation fluids, and any additives. Particularly effective fluids are those described in U. S. Patents 5,551,516; 5,964,295; 5,979,555; 5,979,557; 6,140,277; and 6,258,859. Breakers may also be used for VES's.

In the methods of the Invention that work partially or primarily by the properly timed and located destruction or weakening of a filter cake, the pad and/or the proppant carrying stages preferably also contain a fluid loss control additive or additives to form a suitable filter cake. If they do not contain polymeric materials that can form a suitable filter cake, for example if the fracturing pad and/or carrier fluid are viscosified with a VES, then the pad and/or the proppant carrying stages must contain a fluid loss control additive or additives to form a suitable filter cake. Fluid loss additives can be, by non-limiting example, water-soluble polymers or crosslinked water-soluble polymers. If the pad and/or proppant laden fluids are viscosified with a polymer or cross-linked polymer, the FLA may be the same or a different polymer or crosslinked polymer. The amount needed to viscosify the carrier fluid may be adequate or more may be added to form an appropriate filter cake. FLA's can also be solids such as asbestos, granular starch, calcium carbonate (calcite), particulate mica, plastic particles, solid wax or wax-polymer particles, solid oil-soluble resin particles, insoluble salts, slowly soluble salts (such as sodium chloride if the carrier fluid and formation water have high ionic strengths), and mixtures thereof. The FLA must contain at least one component that can be broken or degraded (for example oxidation of a polymer, or enzymatic degradation of a cross-linked natural polymer) or dissolved (for example dissolution of calcium carbonate by an acid, or dissolution of a wax or resin by a solvent).

The Invention is carried out by determining, sometimes first by experiment and usually finally by computer simulation and modeling, the optimal amounts of FLA and breaker or breakers (optionally with breaker aid) or dissolver (such as acid), and the stages in which they should be included so that the filter cake breaks or dissolves at the desired time and place. One skilled in the art of stimulation of subterranean wells and formations can readily do this with a knowledge of the chemicals and conditions (especially time and temperature) involved. The process can be done for example by adjusting the chemistry and/or the job pumping design or both, including iteratively, usually by modeling until the desired result is predicted. We will call the materials used to break or dissolve filter cakes and/or FLA's "filter cake degradation agents". In some embodiments an FLA may not have been added and the filter cake may have been formed by the viscosifying agent only. In other embodiments, for example when the fluid is viscosified with a VES, the filter cake may have been formed entirely from the FLA or FLA's. In one preferred embodiment, the pad, and optionally the first proppant-laden stages, contain a first breaker and a breaker aid (which could for example be a catalyst) for a second breaker. Subsequent stages contain the second breaker. The breakers and breaker aids

can be solids or liquids, and can be delayed (for example by encapsulation). Intermediate stages could contain both breakers or both breakers plus the breaker aid for the second breaker, or only the second breaker and its breaker aid. Thus the filter cake already contains a breaker aid for the second breaker when the second breaker contacts the filter cake. Thus, the various stages of the job (pad, early proppant stages, late proppant stages) can contain various combinations of FLA, different breakers, and breaker aids for the different breakers. A breaker aid could be pumped before, with, or after the breaker for which it is active. A material that forms a filter cake will always be in the pad, either the viscosifying agent (polymer or crosslinked polymer) or an added FLA. Breaker does not necessarily have to be in the pad, especially if the temperature is high enough for at least some natural degradation to occur. Similarly, an FLA does not necessarily have to be in all of the proppant-containing stages, or any of the proppant-containing stages, if a satisfactory filter cake has already been formed. All of these methods are counter to normal practice, in which it is desirable to maintain fluid efficiency as high as possible until the stimulation job is done.

If the filter cake is to be degraded by dissolution of a component (such as but not limited to calcium carbonate), this can be done by using an acid in the polymer, crosslinked polymer, or VES (all of which are known in the art in combination with acids) in the appropriate stage or stages. Appropriate acids are any acids known in the art for dissolving carbonates, such as, but not limited to, mineral acids like hydrochloric acid, hydrofluoric acid, and mixtures of the two. Organic acids, such as, but not limited to formic acid, acetic acid, fluoboric acid, and citric acid, can also be used, in conjunction with the mineral acids or separately. Additional materials, such as chelating agents, may be used to enhance the dissolution by the acid. Non-limiting examples are aminopolycarboxylic acids such as ethylenediamine tetraacetic acid, diethylenetriamine pentaacetic acid, and mixtures thereof.

This use of acids to dissolve the filter cake during a fracturing job is opposite to what is normally done in conventional fracturing, in which removal of the filter cake during the job is undesirable. For example, there are known methods for acid fracturing in which pad and acid stages are alternated. Each pad stage contains an FLA or polymer or emulsion that forms a filter cake that blocks off regions of the matrix that have already been etched by the acid (or in which wormholes have formed) and diverts the acid to a portion of the matrix that has not previously been attacked by the acid. In such applications, filter cake removal by the acid is undesirable.

It is normally desirable for the filter cake to degrade after stimulation applications in order to reduce the fracture face "skin" damage and to provide maximal flow of fluids from the matrix into the fracture and ultimately into the wellbore. This degradation normally occurs naturally, albeit slowly, by thermal processes, or by dissolution of the filter cake in typical slurry fluids, or by physical processes, in particular due to the reversal of flow (during the treatment flow is out of the fracture and into the formation, and after production begins the flow is out of the formation and into fracture). Filter cake degradation agents have not been used previously to induce very rapid filter cake degradation during hydraulic fracturing treatments. Because deliberate degradation of the filter cake by the methods of the Invention can bring about much faster degradation, it brings about much faster increase in fluid production rates.

One current way to prevent tip screenouts is to design the job so that the fracture is too wide for bridging of the size of proppant being used to occur. Conversely, one way to promote tip screenouts would be to add a material that assists or promotes bridging and stops the movement of proppant in the fracture. We have found that certain materials, when added to a proppant slurry in adequate concentrations, will promote or assist bridging of the proppant particles (by significantly increasing and reinforcing the magnitude of interparticle interactions) and stop the movement of the proppant in the fracture. We term these materials "bridging-promoting materials" or agents. We have found that a tip screenout can be induced during a job, whether or not the job was designed for a tip screenout, by adding the appropriate amount of bridging-promoting materials to the proppant slurry. Although we will discuss this embodiment of the Invention primarily with fibers as an example, other materials could also be used as bridging-promoting agents, such as needles, fibrillated fibers, platelets, irregular particles, shavings, and ribbons, especially but not limited to materials with aspect ratios greater than about three, most preferably greater than about three hundred. Any organic or inorganic, natural or synthetic material is suitable that would decrease the mobility of a fluid/proppant slurry as it dewatered. Materials with aspect ratios greater than about three would be preferred because they would tend to leave a proppant pack with a greater permeability. Particularly suitable, but not limiting, fibers and other materials are described in U. S. Patent Nos. 5,330,005; 5,439,055; 5,501,275; and 5,782,300, which are hereby incorporated by reference. More than one bridging-promoting material may be used in a single treatment, either sequentially or simultaneously. The materials from which the bridging-

promoting agents are made is not a key variable provided that the mobility reducing agents do not chemically interact with other components of the fluids in which they are used, are stable in the environment in which they are used, and they and slurries containing them can be handled, mixed and pumped by the equipment available. The following discussion is based primarily upon using bridging-promoting materials as the way of promoting tip screenouts, but it is to be understood that the concepts of addition of bridging promoting materials and of filter cake formation/degradation may be combined simultaneously or consecutively.

Fibers are used in conventional hydraulic fracturing to prevent proppant flowback, that is, to hold the proppant in the fracture so that it is not produced along with fluids. This allows more aggressive (higher rate) flowback of fracture fluid and of produced hydrocarbon without flowback of proppant. Resin coated proppants were designed to serve the same purpose but fibers are often better. The use of fibers in this way is described in M. Economides and K. Nolte, eds., *Reservoir Stimulation*, 3<sup>rd</sup> edition, John Wiley & Sons, Ltd, New York (2000) pp. 11-30 and 11-31; and in U. S. Patent Nos. 5,330,005; 5,439,055; 5,501,275; and 5,782,300.

The parameters chosen in the use of fibers to control proppant flowback in conventional hydraulic fracturing are selected on the basis of what is desired to occur in the fracture after the treatment is completed. Fiber is added at an optimal concentration to control proppant flowback, while not significantly impacting fracture conductivity. If one is using glass fibers, this concentration is approximately 1 weight per cent by weight of the proppant. This concentration is insufficient to cause bridging during pumping under the conditions at which it is normally employed. In fact, in conventional hydraulic fracturing, the fiber concentration is deliberately selected so as not to increase the bridging tendency during pumping. In most normal hydraulic fracturing situations the fiber is added to the last stages of the treatment, so that the proppant closest to the wellbore is intermingled with fibers. Indeed, in these treatments to prevent proppant flowback, it is most critical that the region of the fracture adjacent to the wellbore is treated. Occasionally in conventional hydraulic fracturing, all the proppant-laden stages are treated with fiber; this may be done in wells where proppant flowback is a most critical issue or when fiber is added for the purpose of reducing friction pressure. However, in these treatments the fiber concentration is scaled linearly with respect to the proppant concentration. (That is, if the amount of proppant is

doubled, the fiber concentration is doubled, etc.) In typical designs, the early proppant stages are relatively low in proppant and fiber; tip screenouts are not desired and if they occur they are not caused by the fibers.

Occasionally, fibers are added throughout a conventional hydraulic fracturing treatment for yet another reason: to assist in proppant transport, for example when fluid viscosity is unusually low. Tip screenouts are avoided in these treatments through careful pre-treatment job design, especially in careful selection of pumping schedules. For example, in these treatments the pad volume is increased over normal job designs to ensure that sufficient fracture width is generated prior to the proppant/fiber slurry entering the fracture. Furthermore, fiber concentrations are carefully tracked in simulated job designs, alerting engineers to the possibility of premature screenouts. Finally, since the addition of fiber is critical to proppant transport in all the stages in such designs, all of the stages must include fiber.

Thus the use of fibers to control proppant flowback when tip screenout is not desired is characterized by two main principles. First, in conventional fracture designs, the amount of fibers needed for flowback control is normally low enough that tip screenout does not occur. Second, although fibers are occasionally added throughout a treatment, for flowback control they are most commonly added at the end of a treatment (or "tailed in"), typically in the last 10 per cent of the operation. This is because it is the physical properties of the proppant pack nearest the wellbore that are of concern and that must be controlled to prevent proppant flowback. The use of fibers to assist in proppant transport in conventional fracturing is characterized by careful job design and monitoring to prevent tip screenouts. In either case when tip screenouts are not desired, they are prevented as best as possible by either the inherent mode of fiber use, or by careful job design.

From this point in the discussion on, with the exception of Example 5, when we refer to "per cent fiber" we mean "weight per cent of the liquid in the slurry". For simplicity, assume that the density of liquids used in fracture fluids is about 8.4 pounds per gallon. A common proppant loading is 8 pounds of proppant per gallon of liquid in the slurry. This would be referred to as 8 pounds proppant added, or 8 PPA. In this case if fiber were added in an amount equal to 1 weight percent of the weight of the liquid, it would be about 0.5 weight percent of the weight of the total

slurry. Thus the amount of fiber when expressed as the weight per cent of the liquid, would be a different per cent of the weight of the slurry, depending upon the amount of proppant.

The treatments of the Invention can be performed in the field in the same way as conventional treatments with the usual equipment, chemicals, and personnel, but with the equipment modified to give the ability to add fiber if that ability is not already present. Methods of adding fiber are described in U. S. patent Nos. 5,501,275; and 5,782,300. Preferred, but not limiting, methods of adding fiber are by adding the fiber to the proppant before it is mixed with the fluid, adding the fiber to the fluid before it is mixed with the proppant, or by adding a slurry of fibers at some stage before the slurry is pumped downhole. Although the fiber is generally added to the fluid at about the same time as the addition of the proppant, it is possible to premix components in advance of a job, or to mix them downhole.

In a preferred method, the treatment is designed to maximize the probability of a tip screenout even if fiber were not present, and, after any additional modifications to the original treatment design that are made after the "data frac" or "mini-frac" to further increase the probability of a tip screenout, the treatment design is yet further modified to include a high concentration of fibers in the fluid. The high concentration of fiber is added at least to the early propped stages of the treatment, when the proppant concentration is from about 0 to about 8 PPA. It is particularly important to ensure that a high concentration of fiber is added to the stages in which the proppant concentration is from about 0.5 to about 6 PPA. Fiber is commonly added throughout the job. As the fiber and proppant concentration increase beyond a critical level, typically aided by an increase in solids concentration due to leak off, a screenout will occur. Since addition of high concentrations of fibers tends to reduce the mobility of the proppant slurry, or even cause an immobile slurry, it is traditionally avoided in conventional hydraulic fracturing; in the present Invention this addition is deliberate. If sand control or proppant flowback control are not needed, it may not be necessary to continue to add fibers after the tip screenout has occurred.

The treatment need not be initially designed to maximize the probability of a tip screenout even if fiber were not present. The treatment could have an otherwise conventional design except for the addition of sufficient bridging-promoting material, such as fibers, to induce a screenout. Furthermore, the fiber addition does not have to be early in the job. It is within the scope of the

Invention to add increasing amounts of fiber (gradually or in steps) until a screenout occurs, or to add fiber later in a job either abruptly at a high enough concentration to cause a screenout or in increasing amounts. It would also be within the scope of the Invention to increase the proppant concentration in the slurry and/or to increase the injection rate in conjunction with adding increasing amounts of fiber or with initiating addition of fiber after pumping fiber-free slurry. Since there will be a greater tendency for screenouts to occur when the leak-off is high, the methods of the Invention could be of greater benefit when leak-off is low. However, the Invention can be used under any conditions in which fracturing, including fracturing/gravel packing is done. For example, factors that affect leak-off, such as the formation permeability or the choice of a leak-off additive or additives, if used, could affect the optimal concentration (or concentration profile) of fibers needed but would not limit there being such an optimal concentration (or concentration profile) of fibers needed.

Combined stimulation/gravel packing with deliberate tip screenout can be done in a variety of ways. Non limiting examples include the following. In the first method, a fracture with a tip screenout is created, then the wellbore is cleaned out, a screen is placed, and a gravel-pack treatment is performed. In the second method the screen and a special tool are placed before the treatment. The tip screenout fracture is formed and packed with the tool set so that injected pad and slurry go into the fracture but not into the annulus; the tool is then set so that slurry enters the annulus. The pumping rate is usually reduced to ensure annular packing. In the third method, instead of gravel and a screen another technique is used to prevent production of proppant or sand. Examples are addition of fibers to the proppant or use of resin-coated proppants just before the end of the fracturing operation. Fibers and resin-coated proppants can also be used with screens.

The methods and fluids of the Invention can also be used in stimulation methods commonly called “water-fracs” or “waterfracs” or “slickwater fracs”. In water-fracs, usually to decrease the cost, as little viscosifier and proppant as possible are used to create a hydraulic fracture. This is accomplished by using very high pump rates and very high total slurry volumes. As usual, in conventional water-fracs the intention is usually to create the longest fracture possible, but if an operator wanted to stop length growth and initiate width growth, a slug of fiber, or of fiber and a higher proppant concentration, could be added.

Fiber, or other bridging-promoting material, may be added in a sufficiently high concentration to induce a tip screenout. However, in another embodiment, bridging-promoting materials need not be added in an amount sufficient to cause a tip screenout in the present Invention, when they are used. The densities of fibers, proppants and fluids each can vary, so the amount of fiber that will be high enough to induce a tip screenout, alone or in conjunction with a filter cake degradation agent, depends upon the specific choices of fibers, proppants and fluids. The following discussion will be in terms of aqueous liquids and preferred fibers of the Invention, synthetic organic polymeric fibers having relatively low densities of from about 1 to about 1.5 grams/cubic centimeter. However, denser fibers, such as those made from inorganic materials such as glass or ceramics, can also be used; such fibers will have densities of up to double or more the densities of synthetic organic polymeric fibers. The amount of fiber in a liquid/fiber/proppant slurry necessary to induce a tip screenout when used in conjunction with a filter cake degradation agent is most closely related to the volume of fiber per volume of fiber/proppant mixture. Thus the amounts of fiber expressed below should be adjusted for the densities of the specific components involved. The higher the density of the fiber, the higher the necessary weight concentration. Also, the aspect ratio, the length, and the diameter of the fiber relative to the diameter of a proppant will affect the amount of fiber (expressed in weight per cent of liquid in the slurry) in a liquid/fiber/proppant slurry necessary to induce a tip screenout. A lower weight per cent of fiber (expressed in weight per cent of liquid in the slurry) will be necessary as the fiber diameter is decreased or the fiber length or aspect ratio are increased. These adjustments are well within the ability of those skilled in the art. Particularly suitable, but not limiting, fibers and other materials are described in U. S. Patent Nos. 5,330,005; 5,439,055; 5,501,275; and 5,782,300, which are hereby incorporated by reference.

What we term "fibers" can be any fibrous material, such as natural organic fibers, comminuted plant materials, synthetic organic fibers (by non-limiting example polyester, polyaramide, polyamide, novoloid or a novoloid-type polymer), fibrillated synthetic organic fibers, glass fibers, carbon fibers, ceramic fibers, inorganic fibers, metal filaments or mixtures thereof. The fibrous material preferably has a length of about 2 to about 30 millimeters and a diameter of about 5 to about 100 microns, most preferably a length of about 2 to about 30 millimeters and a diameter of about 10 to about 100 microns. Fiber cross-sections need not be circular and fibers need not be straight. If fibrillated fibers are used, the diameters of the individual fibrils can be much smaller than the aforementioned fiber diameters.

It has been found that at concentrations of synthetic organic polymer fibers between about 1 to about 2 per cent by weight of liquid, the fiber-containing slurry behaves like a standard fracturing fluid, and can be handled with standard oilfield pumping and blending equipment. It has been tested with downhole tools and it does not plug ports. This addition of the fiber to the early proppant stages will not significantly complicate the execution of the treatment.

However, as the fracture fluid/fiber/proppant mixture enters the formation, the proppant and fiber will concentrate due to fluid leak-off. At higher concentrations the fiber greatly increases the slurry's propensity to bridge. When the fiber concentration is increased to about 4 to about 5 weight per cent by leak-off, the slurry has an appearance of wet pulp. It has been shown in the laboratory and in yard tests that about 4 to about 5 per cent synthetic organic polymer fiber in the liquid can plug a slot 6 to 12 millimeters wide. Therefore, as the fiber and proppant are concentrated in the fracture due to fluid leak-off, the slurry will have a great propensity for the proppant/fiber mixture to bridge and cause a screenout.

If the use of fibers is also planned to aid in inducing a TSO, the fiber is usually in at least the first proppant stages and the concentration is chosen so that the fiber/proppant slurry packs off (is no longer mobile) and causes a TSO when the degradation of the filter cake has proceeded to the point where the fluid efficiency is less than for example about 20%. Note that the amount of fiber needed to cause a TSO in some of the methods of this Invention can be less than the amount of fiber normally used in fracturing to prevent proppant flowback without causing a TSO because in these methods of this Invention, other steps are taken to degrade the filter cake and increase the concentration of the fiber/proppant slurry in the fracture. In other words, bridging is promoted by deliberately enhancing the leak-off. On the other hand, the amount of fiber used may also be more than that normally used for preventing proppant flowback.

The amount of synthetic organic polymer fiber is preferably adjusted over the range from about 0.5 to about 2 weight per cent to account for variations in fluid efficiency. Normally, 0.5 weight percent synthetic organic polymer fiber would not be considered high and would not cause a screenout. However, one object of the Invention is to use a fiber concentration that would result in a screenout. In some cases, for example if the fluid leak-off coefficient is relatively high, and the fluid efficiency low, then the initial fiber concentration could be reduced to about that amount. The concentration might

then be in the "normal" range for a "normal" treatment, but it would be high for the treatment in question. On the other hand, if the fluid efficiency were to be unusually high, then the initial fiber concentration should be increased beyond the typical 2 per cent to induce a tip screenout. Thus the range of synthetic organic polymer fiber concentration of the Invention is from about 0.5 weight per cent of the liquid to about 3 weight per cent, preferably from about 1 weight per cent to about 2 weight per cent. In this context, by "high concentration" we mean a concentration of a specific fiber, in a specific liquid/fiber/proppant combination, high enough to very significantly increase the probability of a screenout under the conditions of the treatment.

Although in conventional hydraulic fracturing the amount of fiber used is normally determined by the amount of proppant used, so that the amount of fiber is changed if the amount of proppant is changed in different stages, in the fluids and methods of this Invention the amount of fiber used is more commonly determined by the amount of liquid used and it is more common to use a constant amount of fiber by weight of liquid.

As fiber stiffness or rigidity increases, so does the propensity to initiate bridging and screenout. However, fluid handling will become more difficult as stiffness increases. Fibers of varying stiffness or rigidity are readily available commercially. Furthermore, friction pressure during pumping often decreases due to the addition of fibers. This is an added benefit particularly in combined fracturing/gravel packing operations where the fluid is often pumped through small ports and passages. The choice of fiber can readily be made by one of ordinary skill in the art by considering the various advantages and disadvantages of different fibers as regards to cost, availability, concentration needed, ease of handling, effect on friction pressure and other factors.

Although we have referred to "tip screenouts" it would be within the scope of the Invention to generate a desired length of conventional fracture with conventional treatment parameters and then induce screenout by beginning addition of filter cake degradation agent and/or filter cake degradation agent aid at high concentration and/or by increasing the fiber concentration. Fiber may also be added to the pad, in amounts comparable to the amounts added to proppant-laden stages. Although fracturing followed by gravel packing is more commonly performed with a screen in place, it is within the scope of the Invention to apply the fluids and methods to treatments that are done without a screen. Although we have described the Invention in terms of hydrocarbon production, it is within the scope of the Invention to use the fluids and methods in wells intended for the production of other fluids such as

water or brine, and in injection, production, or storage wells. Although we have described the Invention in terms of unfoamed fluids, fluids foamed or energized (for example with nitrogen, carbon dioxide or mixtures thereof) may be used; adjustment to the fiber concentration due to any consequent changes in the fluid properties or proppant concentration would be made. It is also to be understood that the fluids and methods of the Invention may be used to cause tip screenouts in multiple fractures, natural fractures, or wormholes or the like created by treatment with acid. Any of the methods of the Invention can be carried out with coiled tubing.

A further advantage to the fluids and methods of the Invention is that they give the operator additional parameters to adjust, that is they afford additional flexibility in designing a treatment that will screen out. Thus in situations in which the operator may not wish to decrease the pad volume, slow the pumps, decrease the proppant loading, or make other design changes, the operator may use one of the methods of this Invention. Thus, in the practice of the Invention, it is preferred to design the treatment so that screenout would probably occur even without the methods of the Invention, and then to add one of the methods of the Invention to the job design in addition to ensure a screenout, but it is equally within the scope of the Invention to design a treatment that probably will not screen out without one of the methods of the Invention, and then to add one of the methods of the Invention to the job design. It is also within the scope of this Invention to design and start pumping a treatment that is not designed or expected to screen out at any point during the treatment and then during the treatment to decide to cause the treatment to screen out and therefore at that point to change the design of the job to incorporate one of the methods of the Invention

It should be pointed out that although it is not desirable for the screenout to occur in the wellbore, in the annulus between a screen (if present) and the wellbore face, or in the perforations, it is desirable that these regions be fully packed at the end of the job. That is, the desired result is to screen off in the fracture (the origination of the screenout is in the fracture) and then to fill (or "pack") the above-mentioned regions with proppant/gravel.

Any proppant (gravel) can be used, provided that it is compatible with the fiber, the formation, the fluid, and the desired results of the treatment. Such proppants (gravels) can be natural or synthetic, coated (for example by resin), or contain chemicals; more than one can be used sequentially or in mixtures of different sizes or different materials. By proppant we mean any particulate material selected for a particular purpose such as propping a fracture to keep it open or gravel packing a

completion to prevent or minimize production of formation fines. Proppants and gravels in the same or different wells or treatments can be the same material and/or the same size as one another. Such materials are usually called proppants when they are placed in fractures and gravel when they are placed in perforations and wellbores, but the term "proppant" is intended to include gravel in this discussion. In general the proppant used will have an average particle size of from about 10 to about 100 U. S. mesh, more particularly, but not limited to 40/60, 20/40, 16/20, 12/20 and 8/20 sized materials. Normally the proppant will be present in the slurry in a concentration of from about 1 PPA to about 25 PPA, preferably from about 1 to about 16 PPA.

Any additives normally used in the pads and proppant-laden stages of such treatments may be included, again provided that they are compatible with the other components and the desired results of the treatment. Such additives can include, but are not limited to anti-oxidants, crosslinkers, corrosion inhibitors, delay agents, biocides and buffers. The wellbores treated can be vertical, deviated or horizontal. They can be completed with casing and perforations or openhole, and with or without screens.

Examples of breakers suitable for use in the method of the present Invention include but are not limited to enzymes such as galactomannanase (for breaking polysaccharides based on galactomannan), enzymes such as alpha-amylase for breaking starches, cellulase and hemi-cellulase for breaking celluloses, and oxidizers such as persulfates, bromates, iodates, permanganates, percarbonates, perchlorates, perborates, hypochlorite, chlorine dioxide, and chlorate (for breaking polymers by oxidation). Additionally, the breakers can be encapsulated to delay their release, as is well known in the art. Encapsulation is advantageous because most or all of the polymer to be broken will be in the filtercake and, with encapsulation, that is where the breaker will be late in the job. If the breaker is not encapsulated, at least some of it will leak off and not be in contact with the polymer in the filtercake, although some may flow back into contact with the polymer when the fracture pressure is released. Encapsulation may also be advantageous because a breaker can be chosen that will break both the polymer and the micelles in the VES if a VES is used. Encapsulation is also advantageous for the delayed reaction it provides. Different breakers are more efficient at different conditions (especially temperature) and for different viscosifiers, as is well known in the art.

Breaker aids (or breaker activators) serve as catalysts to increase the breaker activity and performance, especially at lower bottomhole temperatures. Examples are certain tertiary amines, or mixtures of certain tertiary amines, that are aids for oxidizing breakers, as described in U. S. Patent No. 4,560,486.

It should be understood that breakers and breaker aids may also be included in job designs for the purpose of degrading the viscosifying agent in the carrier fluid. These breakers and breaker aids may be the same as or different from the those included for the purpose of degrading the filter cake. Degradation of the viscosifying agent must occur after degradation of the filter cake, that is the carrier fluid must be capable of transporting proppant until the treatment has been completed. The choice of breakers, and breaker aids, and the timing and concentration of the addition of these and of acid or solvent must be selected accordingly. For example, a slow acting breaker that is insufficiently active to degrade the filter cake during the job but sufficiently active to degrade the viscosifying agent within an acceptable time after pumping has ceased may be added at any point during a job, independent of addition of a filter cake degradation agent or agents or aids. As another example, a breaker aid may be included in the injected fluid during the time in which the filter cake is being laid down so that it is incorporated in the filter cake; a breaker for the viscosifying agent and for the filter cake is added later in the treatment and because of the breaker aid in the filter cake, the filter cake is degraded more rapidly than is the viscosifying agent.

This Invention may be practiced at any formation temperature, taking into account any cool-down that may occur, at which the pad and fracture fluids and their components, in particular the polymer in the pad and the VES and micelles in the fracture fluid, have the needed properties, in particular stability.

Example 1 A tip screenout hydraulic fracturing job was designed and the results that would be obtained were predicted using computer simulations with FracCADE™ (Schlumberger proprietary fracture design, prediction and treatment-monitoring software). The job was designed for a 200 mD permeability sandstone formation 14 feet thick at a depth of 13,715 feet, a bottom hole static pressure of 9500 psi, and a temperature of 118 °C. The proppant used was 20/40 mesh ceramic. The fracturing fluid was viscosified with 30 pounds per thousand gallons of boron-crosslinked guar in 2 per cent KCl. The job design is shown in Table 1. The pump rate is in barrels per minute, the liquid volume is in gallons, the proppant concentration is in pounds of proppant per gallon of liquid and the injection time is in minutes.

<u>Stage Number</u>	<u>Pump Rate</u>	<u>Liquid Volume</u>	<u>Proppant Concentration</u>	<u>Injection Time</u>
1 (Pad)	15	3500	0	5.5
2	15	1143	0.5	1.9
3	15	107	0.5	0.2
4	15	1201	1.5	2
5	15	1148	2.5	2
6	15	1102	3.5	2
7	15	1102	4.5	2.1
8	15	1002	5.5	2
9	15	1003	7.0	2.1
10	15	950	8.5	2.1
11	15	900	10	2.1
12 (Flush)	15	4669	0	7.4

Table 1

FracCADE™ uses the predetermined criteria to determine when a screenout will occur. Two simulations were run for this hydraulic fracturing job. The first was a conventional hydraulic fracturing tip screenout run with no fiber added. For this job, FracCADE™ predicts that screenout will occur when proppant attempts to enter a fracture that is less than 2.5 times the diameter of the proppant, or at 22 PPA, whichever comes first. In the second, a synthetic organic polymeric fiber was added to each proppant stage at a concentration of 0.6 volume per cent of the liquid in the slurry. With the fiber, FracCADE™ predicts that screenout will occur when proppant attempts to enter a fracture that is less than 3.5 times the diameter of the proppant, or at 18 PPA, whichever comes first. This is a comparatively low fiber concentration, so this was a particularly severe test. The results are shown in the following Table 2.

<u>Job Parameter</u>	<u>Without Fiber</u>	<u>With Fiber</u>
Propped Fracture Half Length (feet)	101.1	77.1
Propped Width at Wellbore (inches)	0.348	0.497

Averaged Propped Width (inches)	0.235	0.375
End of Job Net Pressure (psi)	649	1033
Efficiency	0.509	0.533
Effective Conductivity (mD-feet)	1256	1947

Table 2

It can be seen that adding the fiber resulted in a shorter, wider fracture with greater conductivity. The fluid efficiency, reflecting the amount of proppant placed using a given amount of carrier fluid, was greater with the fiber. Without fiber, the proppant packed off at 99 feet after 15 barrels of stage 6 had been pumped. With fiber, the proppant packed off at 76 feet after 22 barrels of stage 4 had been pumped

Example 2 1.5 in. diameter cores were saturated in a test brine (2 gallons per thousand gallons of a 50 per cent solution of tetra methyl ammonium chloride) prior to dynamic fluid loss tests. The dynamic fluid loss apparatus consists of a core holder designed so that fluids can be flowed across one end face of the core (the front end) in such a way that some of the fluid will leak off into the core, and fluids can be injected into the other end (the back end) of the core to measure core permeability; the system is controlled by automation software. Brine was injected into the back end of the core to measure the initial permeability. Dynamic fluid loss was performed by flowing a borate crosslinked guar fluid (at a 20 lb guar/ 1000 gallons of fracturing fluid concentration) across the face of the core for 30 minutes at a differential pressure of about 500 psi. (This results in some flow of fluid into the core, and formation of a filter cake on the core face if there is a filter cake forming material in the fluid.) An automated fracture simulator controlled the injection rate to simulate the shear rate during an actual treatment. The fracture treatment parameters that the dynamic fluid loss experiments were designed to mimic are listed in Table 3. Following dynamic leak-off, the regained permeability was measured by again injecting the same brine into the back end of the core.

<u>Parameter</u>	<u>Treatment Value</u>
Injection Rate	15 bpm

Injection Time	30 min
Power Law Exponent (n')	0.7
Fracture Height	65 ft
Fracture Length	75 ft
Fracture Width (At Wellbore)	0.75 in
Distance From Wellbore	1 ft

Table 3

The experiments were done at 52 °C. Table 4 shows comparisons of laboratory results of dynamic leak-off tests simulating fractures with and without an FLA (the FLA concentration was 30 lbs of fluid loss additive per 1000 gallons of fracturing fluid); this FLA is a mixture of starch and particulate platelets. The data show the effects of the FLA on permeability, leak-off and depth of penetration of leaked-off fluid into the rock. The data show that fluid loss, both spurt (the amount of leak-off before a filter cake is formed) and the leak-off after the filter cake was formed, was much smaller, final permeability was much greater, and matrix penetration depths by fluid were much smaller when the FLA was used. These results show how a good FLA will prevent or delay screenout. The results of tests 2 and 4 are shown graphically in Figure 1. Such data would be used in the design of the methods of the Invention. Figure 2 (not to scale) demonstrates schematically how the presence or absence of a filtercake affects the extent to which fluid leaks off from the fracture into the rock matrix. In Figure 2, a filter cake [1] is formed by the FLA in the upper schematic, but not in the lower, which represents a case in which FLA was not used or was removed. Consequently, without the filter cake, there is more leaked off fluid [2] from the propped fracture [3].

<u>Run</u>	<u>Initial</u> <u>Perm.</u> <u>(mD)</u>	<u>Final</u> <u>Perm.</u> <u>(mD)</u>	<u>Spurt</u> <u>(gal/100ft<sup>2</sup>)</u>	<u>Leak-off after</u> <u>Spurt</u> <u>(gal/100ft<sup>2</sup>)</u>	<u>Penetration</u> <u>Depth</u> <u>(inches)</u>

			(Without FLA)		
1	98	38	146	72	25
2	80	10	123	58	21
			(With FLA)		
3	80	47	46	19	8
4	75	35	60	17	10

Table 4

**Example 3** Figure 3 shows laboratory experiments demonstrating a method of the Invention using two FLA breaker (filter cake degradation agent) stages. These are dynamic fluid loss test runs at 52 °C by the same method as Example 1. It can be seen that in test one when the first half contained an FLA and a first breaker and a breaker aid (filter cake degradation agent aid) for a second breaker that was present in the second half, and there was still FLA in the second half, there was no increase in fluid loss in the second half. In test two, when the first half was like the first half of test one but the second half contained no FLA, there was a dramatic increase in the volume of fluid lost in the second half, indicating that the filter cake had been severely damaged. In a fracture, this would translate into bridging and/or reduced fluid efficiency and a TSO. To ensure that the result was not due solely to the exclusion of the FLA from the second half of test 2, another laboratory test was run (see Figure 4) in which there was no breaker or breaker aid in either stage, but the first stage included the FLA and the second stage did not. Figure 4 shows that in this case there was a slight increase in flow in the second stage, but it was very minor compared to the results shown in the tests in Figure 3. This makes it clear that the major factor was the breakers and especially the inclusion in the first stage of a breaker aid for the breaker in the second stage and that leaving the FLA out of the second stage was of low importance. The first stage of these experiments represents either the pad or the pad plus the early proppant stages of a commercial stimulation treatment; the second stage of these experiments represents the late proppant stages of a commercial stimulation treatment.

**Example 4** Figure 5 demonstrates the effect of adding fiber to promote bridging in addition to adding an FLA and breakers. The figure shows a particular embodiment in which a filter cake with a built-in breaker is created with the pad, then fibers are added to the proppant stage to promote bridging, and then another breaker is added to the later proppant stages. (Schematics A through E of the contents of the fracture are shown from top to bottom as the stimulation progresses; these could be either top views or side views and are not to scale and the fractures are not necessarily the same size in successive schematics.) This sequence stops the fracture growth and then removes the filter cake, which ultimately increases the flow rate, into the fracture, of the fluid to be produced. The viscosifier in the pad, the first filter cake degradation agent, the filter cake degradation agent aid for the second filter cake degradation agent, and the FLA are the same as those in the first half of test 2 of Figure 2; the viscosifier in the carrier fluid is the same as in the pad, and the second filter cake degradation agent is the same as the one in the second half of test 2 in Figure 2. In Figure 5, “2 - 4 PPA” means the stages containing 2 to 4 pounds of proppant per pound of fluid (“pounds proppant added” or PPA) and “4 PPA and Up” means the stages from 4 PPA to the last proppant-containing stage plus a flush.

The viscosified pad contains the first filter cake degradation agent, the filter cake degradation agent aid for the second filter cake degradation agent, and the FLA. As the pad is pumped (schematic A) and is at the leading edge of the growing fracture [4], a filter cake [5] is built for fluid loss control and some fluid leaks off [6] into the formation rock. Enough pad must be pumped for the filter cake to form. In the 2-4 PPA stages (schematic B), the carrier fluid contains a synthetic organic polymeric fiber [7] added to each proppant [8] stage at a concentration of about 0.6 volume per cent of the liquid in the slurry that arrests the fracture length growth. In subsequent stages (schematic C) the second filter cake degradation agent is introduced and begins to degrade the filter cake, aided by the filter cake degradation agent aid (that is already present) for the second filter cake degradation agent. During pumping of the late proppant-laden stages (schematic D) the second filter cake degradation agent degrades the filter cake, causing increasingly greater leak-off. The final result (schematic E) is a relatively short, wide fracture that has screened off when and where desired, has little or no filter cake, and is well-packed with proppant. Many variations on this scheme, for example but not limited to exactly when and how much of each of the FLA, the first filter cake degradation agent, the filter cake degradation agent aid for the second filter cake degradation agent, the second filter cake degradation agent, and the fiber are added are within the scope of the Invention. Other variations may include adding the above materials in different orders or in different combinations.

Example 5 Three fracturing scenarios were simulated with FracCADE™ (Schlumberger proprietary fracture design, prediction and treatment-monitoring software). In these scenarios, the same FLA, and when present the same first filter cake degradation agent, filter cake degradation agent aid for the second filter cake degradation agent, second filter cake degradation agent, and fiber as in Example 3 were used. FLA was added in all three scenarios at a rate designed to form a filter cake of 2 pounds of FLA per one hundred square feet of fracture surface. The job design is shown in Table 5. The pump rate was 15 barrels per minute throughout; the pad and the proppant-laden stages were viscosified with a boron-crosslinked 20 pounds per thousand gallons guar in sea water; the flush contained the same guar at the same concentration in sea water, but uncrosslinked.

<u>Stage</u>	<u>Fluid gallons</u>	<u>Pounds Proppant</u>	<u>Barrels Slurry</u>	<u>Minutes Pumping</u>
PAD	5500	0	131	8.7
0.5 PPA	1000	500	24.3	1.6
1.0 PPA	1000	1000	24.9	1.7
2.0 PPA	1000	2000	26.0	1.7
4.0 PPA	1000	4000	28.1	1.9
6.0 PPA	1000	6000	30.3	2.0
8.0 PPA	1000	8000	32.4	2.2
10.0 PPA	1500	15000	51.9	3.5
12.0 PPA	3000	36000	110.2	7.3
FLUSH	3286	0	78.2	5.2

Table 5

In scenarios 1 and 2, no filter cake degradation agents or filter cake degradation agent aids were used. In scenario 2, fiber was added to the 2 to 4 PPA stages at a rate of 0.8 weight per cent of the proppant. In scenario 3 the pad included a first filter cake degradation agent and a filter cake degradation agent aid for a second filter cake degradation agent, and the proppant-laden stages starting with 2 PPA contained the second filter cake degradation agent. The results of the three simulations are shown in Table 6.

<u>Scenario:</u>	<u>1</u>	<u>2</u>	<u>3</u>
FLA in Pad?	Yes	Yes	Yes
Filter Cake Degradation Agents and Aid Used?	No	No	Yes
Pad Spurt (gal/100ft <sup>2</sup> )	0	0	46
Fiber in 2 – 4 PPA Stages?	No	Yes	No
Proppant Stages Spurt (gal/100ft <sup>2</sup> )	0	0	99
Final Propped Fracture Half Length	55.3	45.4	36.9
Final Propped Fracture Width at Wellbore	1.298	1.729	3.052

Table 6

Note that the design included sufficient pumping time to ensure filter cake formation. Amounts of pad, fracture fluid, fracture fluid viscosifier, breaker (filter cake degradation agent), breaker aid (filter cake degradation agent aid), fluid loss control additive, and proppant typical of commercial treatments were used. It can be seen from scenario 1 that when an FLA was used but no means for destroying the filter cake was employed, a long narrow fracture was produced. When fiber was added to promote a tip screenout in scenario 2, a shorter, wider fracture was created. When filter cake degradation was used to promote the tip screenout, the shortest, widest fracture was created. A good job design would be a combination of scenarios 2 and 3.

The preceding description of specific embodiments of the present Invention is not intended to be a complete list of every possible embodiment of the Invention. Persons skilled in this field will recognize that modifications can be made to the specific embodiments described here that would be within the scope of the present Invention.

## WE CLAIM:

1. A method of causing a screenout in a subterranean formation stimulation treatment, comprising injecting a slurry of a proppant in a carrier fluid above fracturing pressure, comprising adding a bridging-promoting material to the slurry.
2. A method of causing a screenout in a subterranean formation stimulation treatment, comprising injecting a slurry of a proppant in a carrier fluid above fracturing pressure to create one or more fractures, comprising the steps of:
  - a) injecting a pad fluid that forms a filter cake,
  - b) injecting one or more first slurry stages comprising a proppant in a carrier fluid; and
  - c) degrading the filter cake with a filter cake degradation agent while injecting one or more second slurry stages comprising a proppant in a carrier fluid.
3. The method of claim 2 wherein the filter cake is formed from one or more than one of water-soluble polymers, crosslinked water-soluble polymers, fluid loss additives, and mixtures thereof.
4. The method of claim 2 or claim 3 wherein the filter cake degradation agent is selected from the group consisting of oxidizers, enzymes, acids and mixtures thereof.
5. The method of any of claims 2 through 4 wherein the pad fluid comprises a member of the group consisting of fluid loss additives, filter cake degradation agents, filter cake degradation agent aids, and mixtures thereof, provided that no filter cake degradation agent aid is included for a filter cake degradation agent that is included; and the one or more first slurry stages comprise a member of the group consisting of fluid loss additives, filter cake degradation agents, filter cake degradation agent aids, and mixtures thereof, provided that no filter cake degradation agent aid is included for a filter cake degradation agent that is included or was in the pad; and the one or more

second slurry stages comprise a member of the group consisting of filter cake degradation agents, filter cake degradation agent aids, and mixtures thereof.

6. The method of any of claims 2 through 5 wherein the pad fluid and the one or more first slurry stages each comprise a fluid loss additive, a first filter cake degradation agent and a filter cake degradation agent aid for a second filter cake degradation agent that is more active under treatment conditions than is the first filter cake degradation agent; and the one or more second slurry stages contain the second filter cake degradation agent.
7. The method of any of claims 2 through 6 wherein the filter cake comprises a polymer subject to enzymatic and oxidative degradation under treatment conditions; the first filter cake degradation agent is present in the pad and comprises an enzyme that degrades the polymer; the second filter cake degrading agent is present in the one or more second slurry stages and comprises an oxidizing compound that degrades the polymer; and the second filter cake degradation agent aid for the second filter cake degradation agent is present in the pad fluid, the one or more first slurry stages, and the one or more second slurry stages and comprises a tertiary amine.
8. The method of any of claims 2 through 7 wherein the filter cake comprises an acid-soluble solid particulate compound and the second filter cake degrading agent is present in the one or more second slurry stages and comprises an acid capable of dissolving at least part of the acid-soluble solid particulate compound under treatment conditions.
9. The method of any of claims 2 through 8 wherein one or more of the pad fluid, the one or more first slurry stages, and the one or more second slurry stages comprise a bridging-promoting material.
10. The method of any of the preceding claims wherein the wellbore treatment is selected from the group consisting of hydraulic fracturing, hydraulic fracturing followed by gravel packing, and combined hydraulic fracturing and gravel packing.

11. The method of any of the preceding claims wherein a sand control screen is in place before the wellbore treatment.
12. The method of any of the preceding claims wherein the fluid component of the slurry is selected from the group consisting of emulsions, foams, and energized fluids.

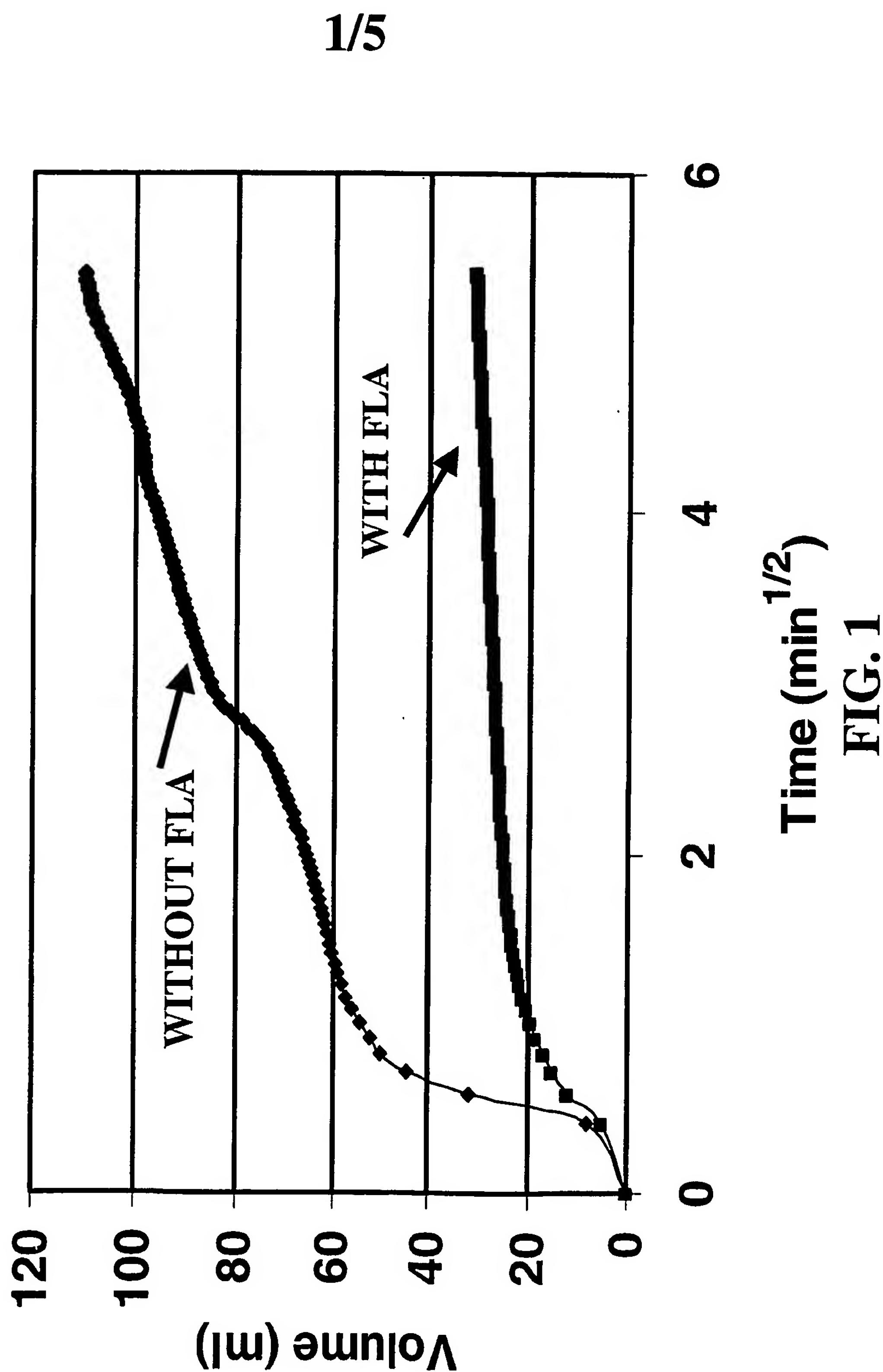
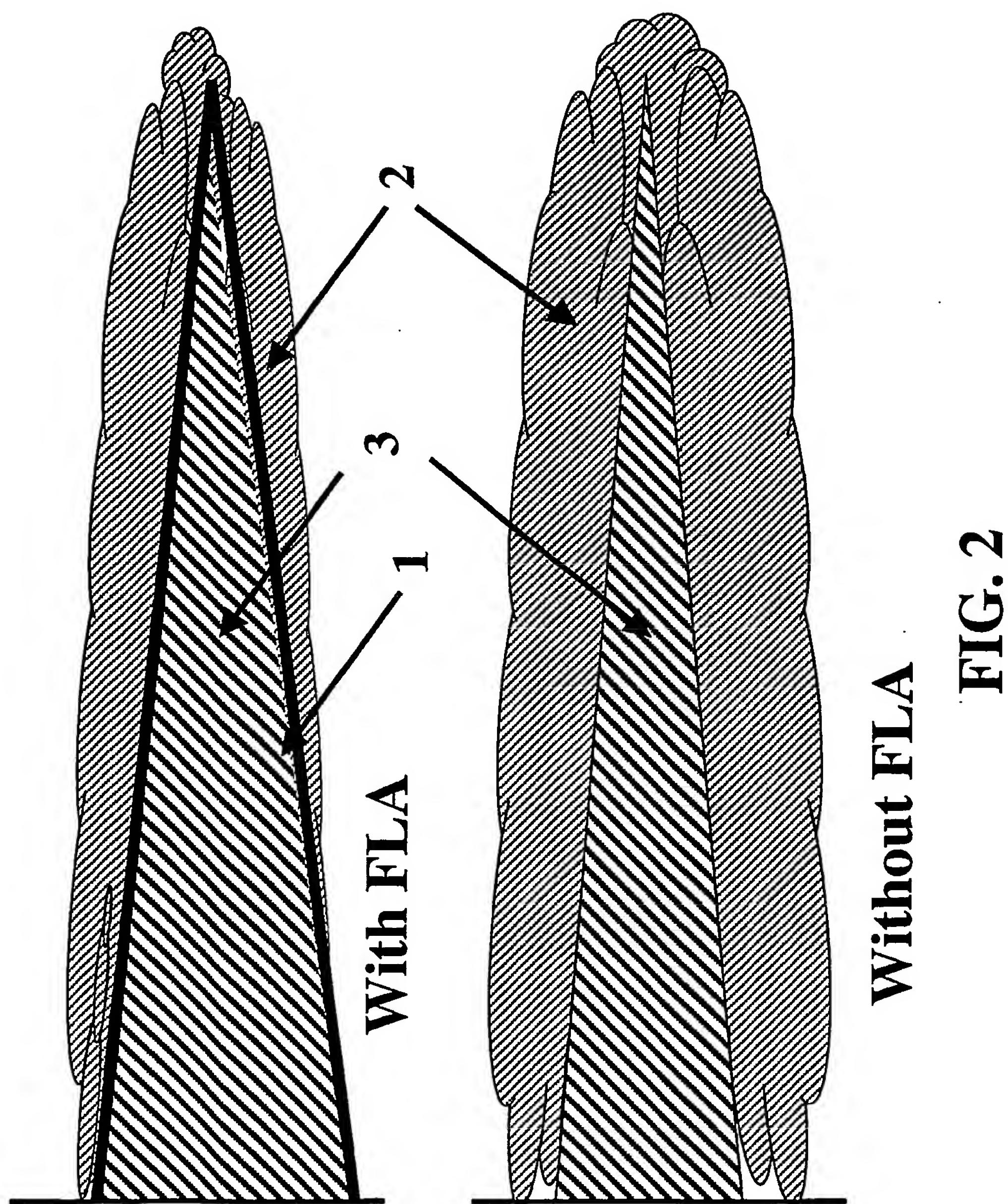


FIG. 1

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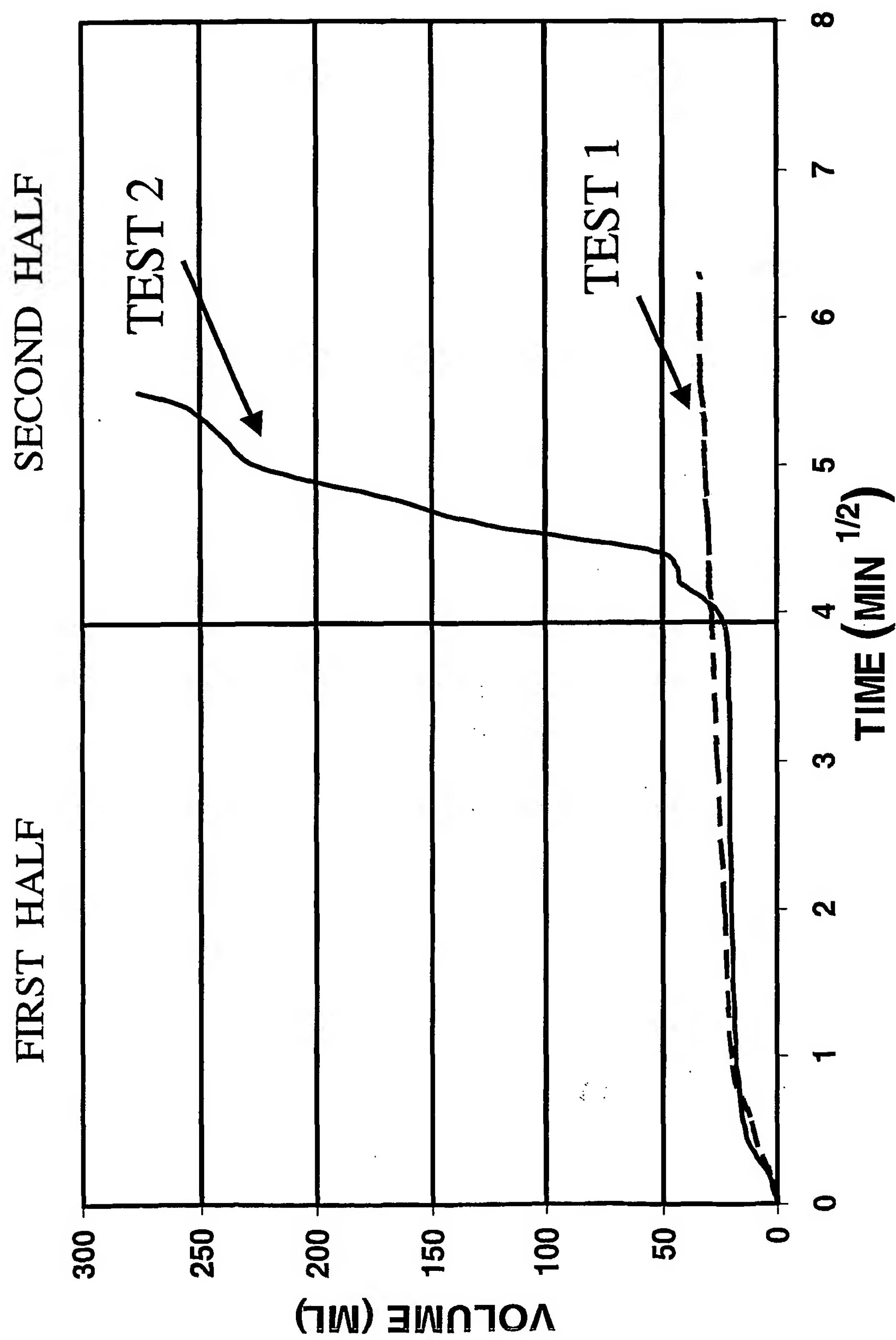


FIG. 3

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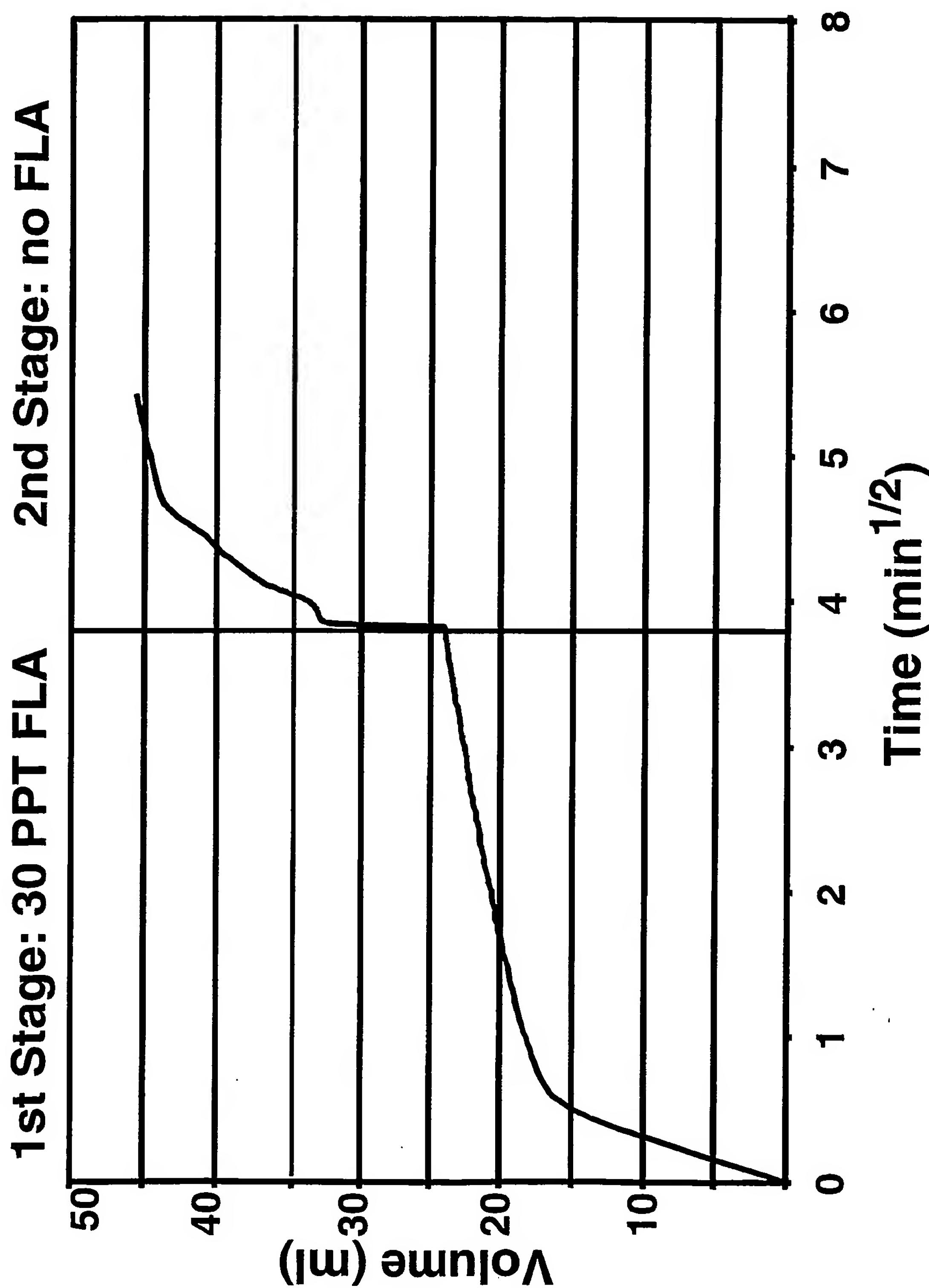


FIG. 4

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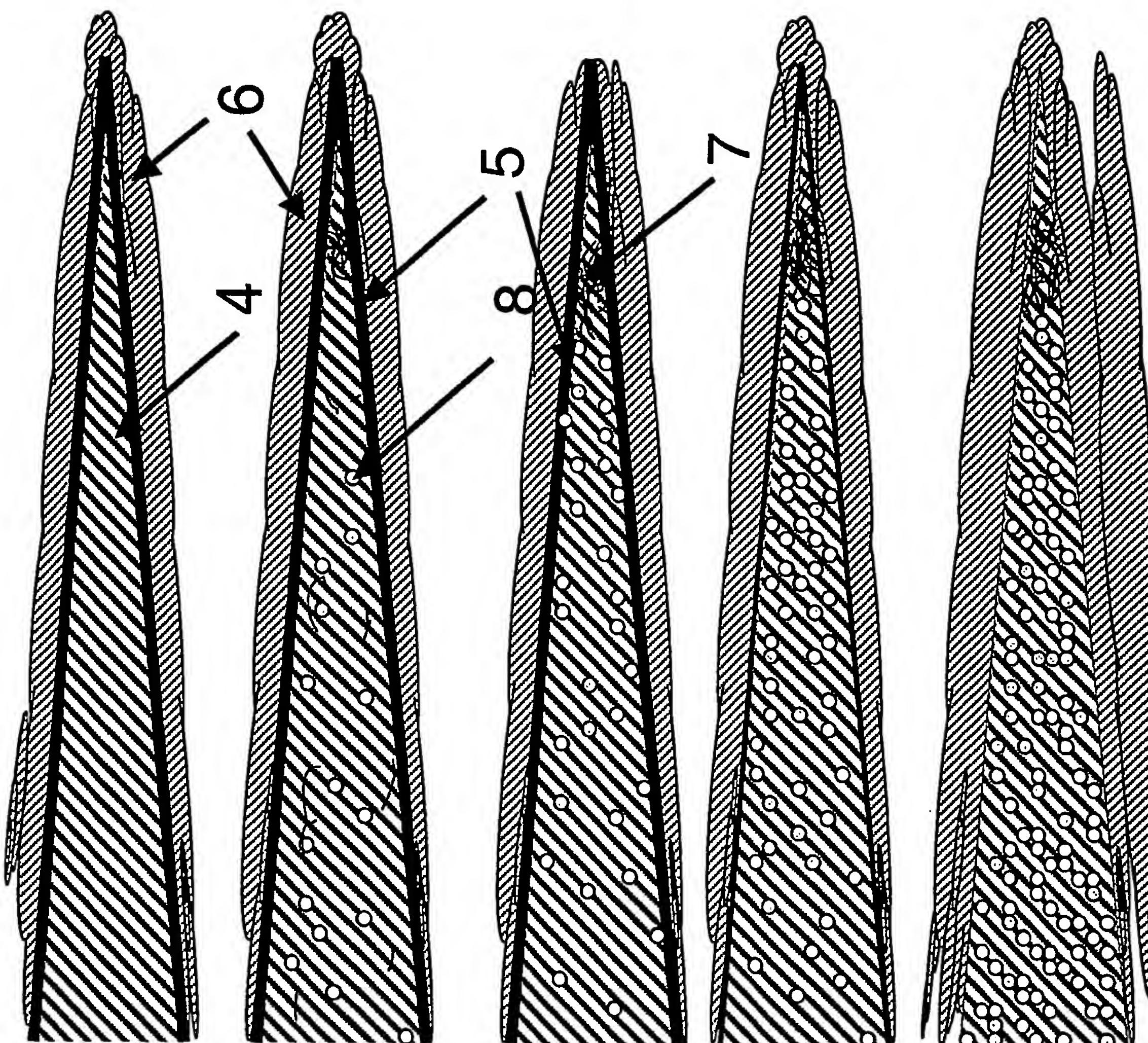


FIG. 5

Schematic  
A: Pad

Schematic B:  
2 - 4 PPA

Schematic C:  
4 PPA and Up

Schematic D:  
Later  
Proppant  
Stages

Schematic E:  
Final Desired  
Result

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(71) Applicant (for CA only): SCHLUMBERGER CANADA LIMITED [CA/CA]; Eau Claire Place I, 525 3rd Avenue, SW, Alberta, Alberta T2P004 (CA).

(71) Applicant (for FR only): COMPANIE DES SERVICES DOWELL SCHLUMBERGER S.A. [FR/FR]; 50, Avenue Jean Jaures, F-F-92120 Montrouge (FR).

(71) Applicant (for AM, AT, AZ, BY, DE, DK, HR, IT, KG, KP, KR, KZ, MD, NO, NZ, PL, RO, RU, TJ, TM, UA, ZA only): SCHLUMBERGER TECHNOLOGY B.V. [NL/NL]; Parkstraat 83-89, NL-2514 JG The Hague (NL).

(71) Applicant (for GB, JP, NL only): SCHLUMBERGER HOLDINGS LIMITED [—/—]; P. O. Box 71, Craigmuir Chambers, Road Town, Tortola (VG).

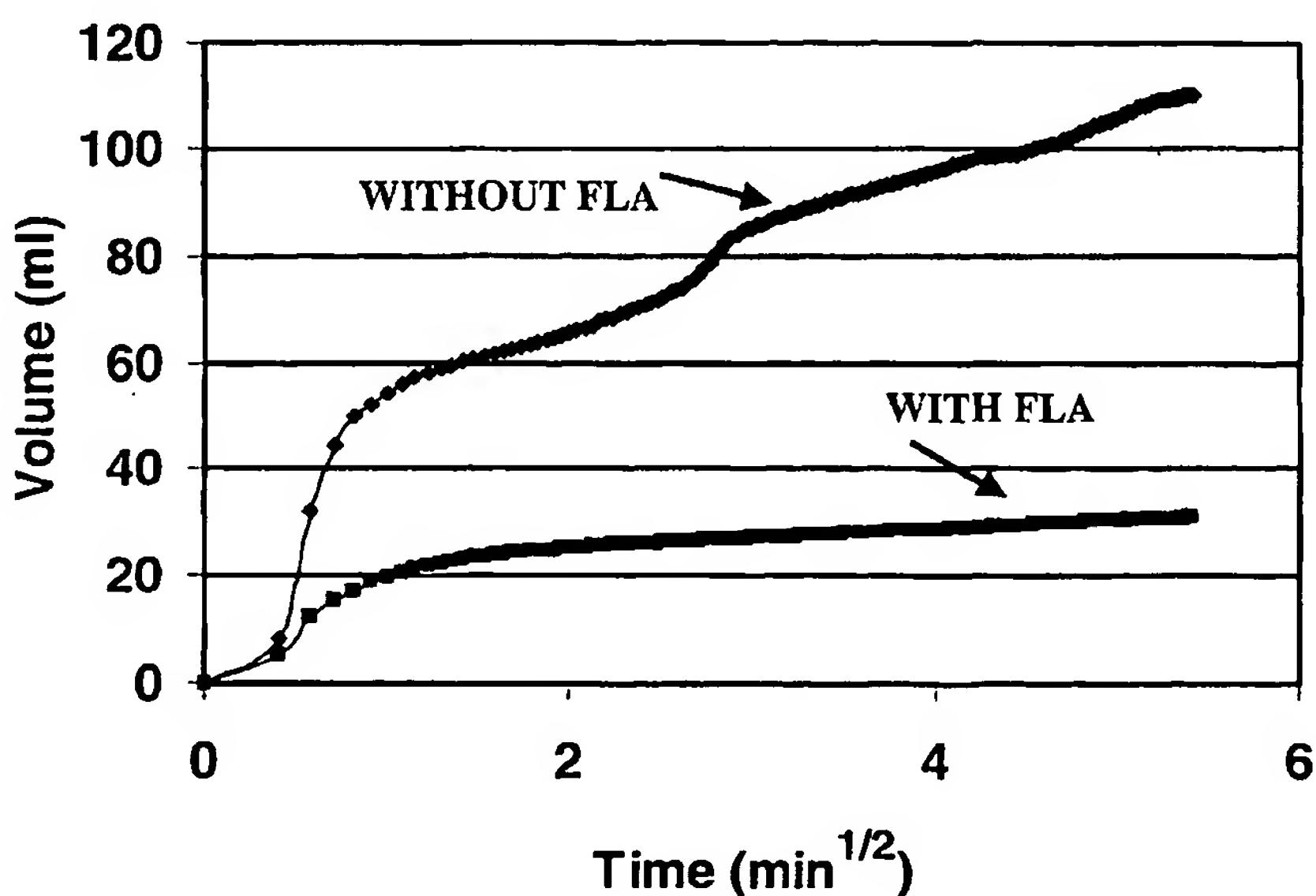
(72) Inventors: BONEY, Curtis, L.; 14918 Chadbourne, Houston, TX 77079 (US). WILLBERG, Dean; 3214 Lakefield Way, Sugar Land, TX 77479 (US). MILLER, Matthew, J.; 3054 La Quinta Drive, Missouri City, TX 77459 (US).

[Continued on next page]

(54) Title: METHODS FOR CONTROLLING SCREENOUTS



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(57) Abstract: Methods are presented to induce a screenout during a subterranean formation fracturing or combined fracturing and gravel packing treatment by laying down a filter cake early in the treatment, then injecting proppant slurry, and then while proppant slurry injection continues chemically damaging the filter cake with one or more filter cake degradation agents, and optional filter cake degradation agent aids, so that leak-off increases, the concentration of proppant in the fracture increases, and the proppant screens out. The additional use of bridging-promoting materials, alone or in conjunction with filter cake degradation, is included.



(74) **Agent:** MENES; Etudes et Productions Schlumberger, 1, rue Henri Becquerel, BP 202, F-92142 Clamart (FR).

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Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

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C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	US 5 722 490 A (EBINGER CHARLES D) 3 March 1998 (1998-03-03) column 1, line 26 -column 2, line 23 ---	1
X	US 5 908 073 A (NGUYEN PHILIP D ET AL) 1 June 1999 (1999-06-01) column 1, line 13 -column 1, line 60 ---	1
X	US 5 325 921 A (JOHNSON MICHAEL H ET AL) 5 July 1994 (1994-07-05) column 1, line 7 -column 4, line 58 column 5, line 1 -column 10, line 5 ---	1-4
Y	US 6 076 046 A (MANIERE JEROME ET AL) 13 June 2000 (2000-06-13) column 1, line 19 -column 4, line 60 ---	5-12
Y	US 6 076 046 A (MANIERE JEROME ET AL) 13 June 2000 (2000-06-13) column 1, line 19 -column 4, line 60 ---	5-12
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European Patent Office, P.B. 5818 Patentlaan 2  
NL - 2280 HV Rijswijk  
Tel. (+31-70) 340-2040, Tx. 31 651 epo nl,  
Fax: (+31-70) 340-3016

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Y	US 5 783 527 A (DOBSON JR JAMES W ET AL) 21 July 1998 (1998-07-21) column 1, line 40 -column 4, line 26 ---	2-12
Y	US 5 247 995 A (TJON-JOE-PIN ROBERT M ET AL) 28 September 1993 (1993-09-28) column 1, line 30 -column 6, line 22 ---	2-12
P,Y	US 6 494 263 B2 (TODD BRADLEY L) 17 December 2002 (2002-12-17) column 1, line 31 -column 2, line 61 ---	5-12
A	HALL B E ET AL: "SUCCESSFUL FRAC PACKS REQUIRE CAREFUL PLANNING" OIL AND GAS JOURNAL, PENNWELL PUBLISHING CO. TULSA, US, vol. 98, no. 14, 3 April 2000 (2000-04-03), pages 37-38, 40-41, 44, XP000969504 ISSN: 0030-1388 the whole document ---	1,2
A	US 6 172 011 B1 (CONSTIEN VERNON G ET AL) 9 January 2001 (2001-01-09) column 1, line 15 -column 4, line 17 ---	1,2
A	US 6 192 985 B1 (ENGLAND KEVIN W ET AL) 27 February 2001 (2001-02-27) column 1, line 46 -column 5, line 42 -----	1,2

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Information on patent family members

International Application No

PCT/EP 02/10126

Patent document cited in search report		Publication date		Patent family member(s)	Publication date
US 5722490	A	03-03-1998	US	5755286 A	26-05-1998
US 5908073	A	01-06-1999	NONE		
US 5325921	A	05-07-1994	AU EP NO WO US	5353394 A 0616660 A1 933774 A 9409254 A1 5504062 A	09-05-1994 28-09-1994 22-04-1994 28-04-1994 02-04-1996
US 6076046	A	13-06-2000	NONE		
US 5783527	A	21-07-1998	US AU AU CA DE DE DK EP NO	5607905 A 689842 B2 1472295 A 2140845 A1 69517223 D1 69517223 T2 672740 T3 0672740 A1 950946 A	04-03-1997 09-04-1998 21-09-1995 16-09-1995 06-07-2000 22-02-2001 07-08-2000 20-09-1995 18-09-1995
US 5247995	A	28-09-1993	US US CA GB NL NO WO DE DE DK EP WO DE DK EP WO	5201370 A 5224544 A 2139624 C 2283519 A , B 9320040 T 950063 A 9401654 A1 69316342 D1 69316342 T2 628130 T3 0628130 A1 9317218 A1 69318013 D1 628129 T3 0628129 A1 9318278 A1	13-04-1993 06-07-1993 02-01-2001 10-05-1995 01-05-1995 14-02-1995 20-01-1994 19-02-1998 27-08-1998 14-09-1998 14-12-1994 02-09-1993 20-05-1998 18-01-1999 14-12-1994 16-09-1993
US 6494263	B2	28-03-2002	US US BR EP NO BR EP NO US	6422314 B1 2002036088 A1 0200033 A 1223207 A1 20020058 A 0103170 A 1178099 A2 20013746 A 2002139532 A1	23-07-2002 28-03-2002 22-10-2002 17-07-2002 10-07-2002 26-03-2002 06-02-2002 04-02-2002 03-10-2002
US 6172011	B1	09-01-2001	US US US AU CA NO AU AU CA	5501275 A 5439055 A 5330005 A 6805496 A 2188098 A1 964256 A 679711 B2 5790894 A 2119316 A1	26-03-1996 08-08-1995 19-07-1994 11-09-1997 09-09-1997 09-09-1997 10-07-1997 06-10-1994 06-10-1994

## INTERNATIONAL SEARCH REPORT

Information on patent family members

International Application No

PCT/EP 02/10126

Patent document cited in search report	Publication date		Patent family member(s)	Publication date
US 6172011	B1		NO 941182 A	06-10-1994
			DE 69429739 D1	14-03-2002
			DE 69429739 T2	12-09-2002
			DK 619415 T3	21-05-2002
			EP 0619415 A2	12-10-1994
<hr/>				
US 6192985	B1	27-02-2001	AU 1095100 A	12-07-2000
			EA 2464 B1	25-04-2002
			EP 1165936 A1	02-01-2002
			NO 20013022 A	17-08-2001
			WO 0037777 A1	29-06-2000
<hr/>				